

Influence of dissolved organic matter on the removal of 12 organic micropollutants from wastewater effluent by powdered activated carbon adsorption

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Ronan Guillossou, Julien Le Roux, Romain Mailler, Caroline Soares Pereira-Derome, Gilles Varrault, et al.. Influence of dissolved organic matter on the removal of 12 organic micropollutants from wastewater effluent by powdered activated carbon adsorption. Water Research, 2020, 172, pp.115487. 10.1016/j.watres.2020.115487. hal-02433266

HAL Id: hal-02433266 https://enpc.hal.science/hal-02433266

Submitted on 28 Jun 2020

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1 Title

- 2 Influence of dissolved organic matter on the removal of 12 organic micropollutants from
- 3 wastewater effluent by powdered activated carbon adsorption

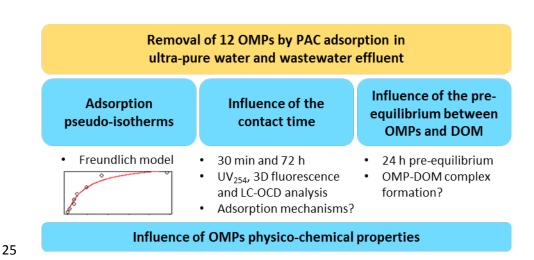
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18 Highlights

- OMPs removal was lower in WWTP effluent than ultra-pure water due to DOM
- 20 adsorption
- Pore blockage was the main negative effect rather than competition for adsorption sites
- OMPs charge had an impact on their adsorption rate in presence of wastewater
- A pre-equilibrium between OMPs and DOM decreased DOM negative effects

24 Graphical abstract



Abstract

The presence of dissolved organic matter (DOM) in wastewater effluents is recognized as the main factor limiting the adsorption of organic micropollutants (OMPs) onto activated carbon. The degree of the negative effect that DOM, depending on its quality, exerts on OMPs adsorption is still unclear. The influence of the interactions between DOM and OMPs on their removal is also not fully understood. Adsorption isotherms and conventional batch tests were performed in ultra-pure water and in wastewater effluent to study the influence of DOM on the adsorption of 12 OMPs onto powdered activated carbon. Best fit of adsorption pseudo-isotherms was obtained with the Freundlich equation and showed, as expected, that OMPs adsorption was higher in ultra-pure water than in wastewater effluent due to the presence of DOM leading to pore blockage and competition for adsorption sites. LC-OCD analysis revealed that biopolymers and hydrophobic molecules were the most adsorbed fractions while humic acids were not removed after a contact time of either 30 min or 72 h. The presence of DOM had a negative impact on the removal of all OMPs after 30 min of adsorption, but similar removals to ultra-pure water were obtained for 6 OMPs after 72h of adsorption. This demonstrated that competition between DOM and OMPs for adsorption

sites was not a major mechanism as compared to pore blockage, which only slowed down the adsorption and did not prevent it. The charge of OMPs had a clear impact: the adsorption of negatively charged compounds was reduced in the presence of wastewater effluent due to repulsive electrostatic interactions with the adsorbed DOM and the PAC surface. On the other hand, the removal of positively charged compounds was improved. A 24h preequilibrium between OMPs and DOM improved their removal onto PAC, which suggest that OMPs and DOM interact in solution which decreased the negative effects caused by the presence of DOM, e.g. through co-adsorption of an OMP-DOM complex.

Keywords

- 51 Wastewater advanced treatment; Organic micropollutants; Dissolved organic matter;
- 52 Activated carbon adsorption.

1. Introduction

The presence of organic micropollutants (OMPs) in aquatic bodies is a concern due to their potential persistence and suspected negative effects on ecosystems (Courtier et al., 2019; Desbiolles et al., 2018; Zenker et al., 2014). One of the main sources of OMPs are wastewater effluents since wastewater treatment plants (WWTPs) are not designed for their removal (Yang et al., 2017). Some compounds can however be well removed during the biological treatment (e.g. acetaminophen, ibuprofen, ketoprofen or naproxen), but their concentrations in the wastewater effluent is still an issue (ranging from ng/L levels up to tens or even hundreds of μg/L) (Guillossou et al., 2019; Jelic et al., 2011; Joss et al., 2005; Verlicchi et al., 2012). Different processes commonly employed to eliminate OMPs for drinking water production (e.g. activated carbon adsorption or oxidation processes such as ozonation) are gaining interest for wastewater treatment (Altmann et al., 2014; Bourgin et al., 2018; Margot et al., 2013). Activated carbon adsorption offers the advantage of being

able to remove a wide range of compounds, and of being easy to use and flexible, with no risk of toxic byproducts generation (Kårelid et al., 2017; Mailler et al., 2016a, 2015; Meinel et al., 2015).

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Adsorption is a complex process driven by the properties of OMPs and the properties of activated carbon, and is also influenced by the water quality, mainly the presence of dissolved organic matter (DOM). Some authors proposed that activated carbon adsorption was driven by the hydrophobicity of OMPs (de Ridder et al., 2010; Westerhoff et al., 2005) but this was mostly observed for neutral compounds and not for charged compounds (de Ridder et al., 2011; Kovalova et al., 2013; Mailler et al., 2015; Margot et al., 2013). DOM affects the adsorption of OMPs onto activated carbon through direct competition for available surface/adsorption sites and pore blockage, depending on its nature (i.e. average molecular weight, hydrophobicity) and the activated carbon porosity (Newcombe et al., 1997). Newcombe et al. (2002) reported that low molecular weight DOM (≈ 200 Da) reduced the equilibrium adsorption capacity of 2-methylisoborneol by competition for adsorption sites and blockage of micropores. The medium (200-600 Da) and high molecular weight DOM (> 1000 Da) could not access micropores but reduced the adsorption rate by restricting direct access to adsorption sites through macro- and mesopores, necessitating a more tortuous diffusion path for 2-methylisoborneol. OMPs can also interact through electrostatic attraction/repulsion, van der Waals, π - π or hydrogen bonds with the DOM. Interactions between DOM and OMPs in the dissolved phase were observed during the treatment of effluents by membrane filtration, leading to an increase of OMPs rejection (Majewska-Nowak et al., 2002; Tödtheide et al., 1997). Many studies have been conducted on the interactions between pesticides and DOM (Caupos et al., 2015; Ilani et al., 2005; Lee et al., 2003), but little data is available for other OMP families such as pharmaceuticals. Hernandez-Ruiz et al. (2012) demonstrated that bisphenol-A could interact with microbial

byproduct-like and humic acid-like DOM components from wastewater, and carbamazepine and ibuprofen with fulvic acid-like components. The influence of these interactions on the adsorption by activated carbon has been barely studied, especially with wastewater DOM. Jin et al. (2018) observed that zwitterionic compounds could interact with humic acids in solution, be adsorbed onto activated carbon and also interact with humic acids adsorbed on the activated carbon surface. The presence of humic acids increased the removal of tetracycline and ciprofloxacin thanks to interactions with humic acids which trapped OMPs. However, these interactions between OMPs and DOM were observed under specific conditions (low dose of activated carbon and very high concentrations of DOM and OMPs) that are not representative of the real conditions encountered in drinking water plants or wastewater treatment plants.

Only a few studies were conducted to assess the influence of DOM originating from wastewater effluents on the adsorption of OMPs onto activated carbon. Wastewater DOM is a complex mixture, generally considered to be composed of large organic molecules (biopolymers, humic substances and building blocks) and smaller molecules (low molecular weight acids and neutrals) (de Ridder et al., 2011; Pernet-coudrier et al., 2008). Some authors proposed that the main negative effect of DOM was the competition for adsorption sites rather than pore blockage: Zietzschmann et al. (2014) fractionated DOM using nanofiltration and obtained a lower adsorption of 5 OMPs in the presence of low molecular weight DOM (competition for adsorption sites phenomenon) compared to raw and high molecular weight DOM (pore blockage phenomenon). They reported that the impact of the small DOM molecules was more important for medium and weakly adsorbing OMPs. Moreover, the DOM adsorbed onto the activated carbon is globally negatively charged at the pH of the wastewater and can decrease the adsorption of negatively charged OMPs through repulsive electrostatic interactions (de Ridder et al., 2011). A negative influence of DOM on

the adsorption of negatively charged compounds was also observed by Hu et al. (2016). Alves et al. (2018) reported that in the absence of DOM, the textural properties (i.e. the porosity) of micro-grain activated carbons (µGACs) played the most important role in the adsorption of OMPs, while in the presence of DOM the surface chemistry of µGACs (i.e. point of zero charge, surface functional groups) had a predominant impact and positively charged compounds were better removed.

While the negative effect of DOM on OMPs adsorption is known, the degree of this effect (i.e. quantification of the decrease in adsorption rates) in relation to the DOM composition is still unclear. The influence of OMPs-DOM interactions on OMPs adsorption is also not fully understood and was not comprehensively studied in conditions close to realistic wastewater treatment applications (i.e. synthetic water, low OMPs concentrations and activated carbon doses). In this context, the present work evaluated the adsorption of 12 OMPs onto powdered activated carbon (PAC) under various conditions by following 3 approaches. As a first step, short-term adsorption capacity at various concentrations of the 12 OMPs (i.e. pseudoisotherms) was evaluated in two different matrices (ultra-pure water and wastewater effluent) to assess the influence of DOM on OMPs removal. Batch tests in ultra-pure and wastewater effluent were then performed at short and long contact times with PAC (30 min and 72 h) to compare the short-term capacity with a long-term adsorption equilibrium and thus to characterize the underlying adsorption mechanisms. DOM adsorption was examined in parallel through LC-OCD, UV₂₅₄ and fluorescence excitation/emission analyses to better understand its adsorption and its effect on OMPs removal. Finally, the influence of a preequilibrium between OMPs and DOM before adsorption was examined to study the possible interactions between OMPs and DOM. The links between OMPs physico-chemical properties and their adsorption were discussed for each experiment.

2. Materials and methods

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2.1. Materials

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Wastewater effluent samples were punctually collected from the Seine Centre WWTP (SIAAP, Colombes, France), treating wastewater of about 800,000 inhabitant equivalents with a flow of 240,000 m³/day. After pre-treatment (screening, grit and oil removal), a physico-chemical lamellar settling unit removes particles and colloids, 3 biofiltration stages remove nutrients then the effluent is discharged into the Seine river (Rocher et al., 2012). The pH of the wastewater effluent ranges from 7.8 to 8 (SIAAP data). The PAC used for all adsorption experiments was PB-170 (DaCarb, see physico-chemical properties summarized in Table S1) and was previously studied in a large-scale pilot and in batch experiments (Mailler et al., 2016b, 2015). Organic micropollutants were purchased from Sigma-Aldrich and their physico-chemical properties are described in Table 1 (molecular weight, hydrophobicity/log D and charge) and Table S2 (van der Waals volume, minimal projection area, polar surface area and hydrogen bonds).

2.2. Experimental methods

- The 12 employed OMPs (Table 1) were selected based on their occurrence and
- 156 concentrations in Parisian wastewater effluents (Mailler et al., 2015). They were commonly
- found in WWTP effluents and present a broad range of physical and chemical properties (i.e.
- charge, size, hydrophobicity).
- 159 Short-term adsorption capacity of the 12 OMPs was studied after 30 min at room
- temperature (20 °C) and at 8 different concentrations (ranging from 0.04-1.7 μg/L to 1.2-52
- 161 µg/L depending on the OMPs, concentrations C1-C8 in Table S3) in ultra-pure water (pH
- adjusted to 8.0) and wastewater effluent, resulting in pseudo-isotherm curves (since an
- adsorption isotherm is assumed to be obtained at reaction equilibrium, which was not

reached after 30 min) (experiment 1). The Freundlich equation (Freundlich, 1906) was used to model adsorption pseudo-isotherms (Equation 1):

$$166 q_t = K_F C_t^{\frac{1}{n}}$$

167 (1)

where q_t (µg/mg) is the amount of adsorbate uptake, K_F (µg/mg)/(µg/L)^{1/n} is the Freundlich constant, C_t (µg/L) is the adsorbate concentration and 1/n (dimensionless) is the Freundlich intensity parameter related to the intensity of the adsorption driving force or the surface heterogeneity.

The modeling parameters (K_F and 1/n) and p-values from the Student test were obtained for each OMP and each matrix (ultra-pure water or wastewater effluent) via non-linear least squares regression with the nlstools package (Baty et al., 2015) using R software (R Core Team, 2007).

Table 1. Name, type and main physico-chemical properties of OMPs used in this study. LOQ: limit of quantification (ng/L); MW: molecular weight (g/mol); $\log K_{ow}$: partition coefficient between water and octanol (MarvinSketch, ChemAxon); $\log D$: $\log K_{ow}$ at pH = 8.0. Charge: average charge based on the presence percentage of each OMP species (anionic, cationic, neutral, zwitterionic) at pH 8 (MarvinSketch, ChemAxon).

Compound	Туре	LOQ (ng/L)	MW	Log D (pH = 8)	Charge (pH = 8)	
1			(g/mol)	<i>E</i> 4 ,		
Acetaminophen	Analgesic	0.5	151	0.90	-0.03	
Atenolol	Beta-blocker	1	266	-1.25	0.98	
Carbamazepine	Anticonvulsant	1	236	2.77	0.00	
Diclofenac	Analgesic	0.5	296	0.26	-1.00	
Erythromycin	Antibiotic	4	734	2.07	0.71	
Ibuprofen	Analgesic	6	207	0.69	-0.99	
Lorazepam	Antidepressant	1.5	321	3.53	0.00	
Ofloxacin	Antibiotic	1	361	-1.12	-0.99	
Oxazepam	Antidepressant	2	287	2.92	0.00	
Roxithromycin	Antibiotic	0.5	837	1.89	0.92	
Sulfadiazine	Antibiotic	1	250	-0.66	-0.91	
Trimethoprim	Antibiotic	2	290	1.22	0.12	

The influence of contact time was studied by conducting comparative adsorption tests in ultra-pure water and wastewater effluent during 30 min and 72 h at an average OMPs concentration (0.48-20 µg/L depending on the OMPs, concentration C5 in Table S3)

(experiment 2). DOC, DOM fractions from LC-OCD chromatograms, UV_{254} and the intensity of 6 fluorescence indexes from excitation/emission matrices were determined before and after adsorption.

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Finally, adsorption experiments were performed with and without a 24 h pre-equilibrium between the wastewater effluent and spiked OMPs (at the lowest working concentrations, i.e. 0.04- $1.7 \mu g/L$ depending on the OMPs, concentration C1 in Table S3) to study the influence of the contact between DOM and OMPs prior to adsorption (during 30 min and 72h) (experiment 3).

A dose of 10 mg/L of PAC was added to the working solutions during all the experiments. This dose was previously demonstrated to maximize differences between molecules in terms of removal, which allows the observation of relationships between physico-chemical properties of OMPs and their removal (Mailler et al., 2016b). Experiments were conducted only one time because previous results indicated that the variability of OMPs removal was low (<10%) in similar conditions (Guillossou et al., 2020). Batch systems were placed under strong stirring during the required contact time. Pre-determined volumes of the stock solution containing the 12 OMPs were spiked in working solutions of 1.5 L to reach the targeted concentrations for each experiment. Volumes of the spiked solution were chosen to maintain a low percentage of solvent (methanol) added to the working solution (< 0.05%). The targeted concentrations of OMPs in the working solution were chosen to ensure that all OMPs were not completely adsorbed onto the PAC after the chosen contact times and that residual concentrations were above limits of quantification (LOQ, Table 1). Unless specifically mentioned, OMPs were always spiked in the wastewater effluent 24 h prior to PAC addition to simulate the interactions between DOM and OMPs occurring during sewer transfer and inside WWTPs.

2.3. Analytical procedures

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OMPs were analyzed within 48 h at the Institute of Analytical Sciences (ISA – Villeurbanne, France) by liquid chromatography coupled to tandem mass spectroscopy. Prior to analysis, all samples were homogenized and filtered on 0.7 µm GF/F glass filters (Whatman). More information on the analytical methods can be found in the literature (Vulliet et al., 2011). LOQs of the 12 OMPs ranged between 0.5 and 6 ng/L (Table 1). If the concentration of some pharmaceuticals was below the LOQ after adsorption, their removal from the liquid phase and the quantity adsorbed onto the solid phase were estimated as if their concentration was equal to LOQ/2. Dissolved organic carbon (DOC) was analyzed for each experiment by the certified SIAAP laboratory filtration on 0.45 µm polyvinylidene fluoride filters (Milex®, Merck) (limit of quantification = 0.3 mgC/L). Liquid size-exclusion chromatography was coupled with organic carbon detection (LC-OCD, DOC-Labor Dr. Huber, Germany) to study the adsorption of different DOM fractions including biopolymers, humic acids, building blocks and low molecular weight acids and neutrals (Huber et al., 2011). Spectroscopic measurements were performed for experiment 2 and 3 at room temperature directly after sampling and filtration on 0.45 µm polyvinylidene fluoride filters (Milex®, Merck). UV₂₅₄ was measured in a 1 cm quartz cuvette using a spectrophotometer (Genesys 10S UV-Vis, Thermo Scientific). Fluorescence emission-excitation matrices (EEMs) were obtained using a 1 cm quartz cuvette and a spectrofluorometer (FP-8300, 150-W Xenon lamp, Jasco) with excitation wavelengths ranging from 240 nm to 450 nm with an interval of 5 nm, and emission wavelengths ranging from 250 nm to 600 nm with an interval of 2 nm. When UV_{254} was higher than 0.080 1/cm, the samples were diluted with ultrapure water to avoid inner filter effects due to adsorbing species present in the wastewater (Alberts and

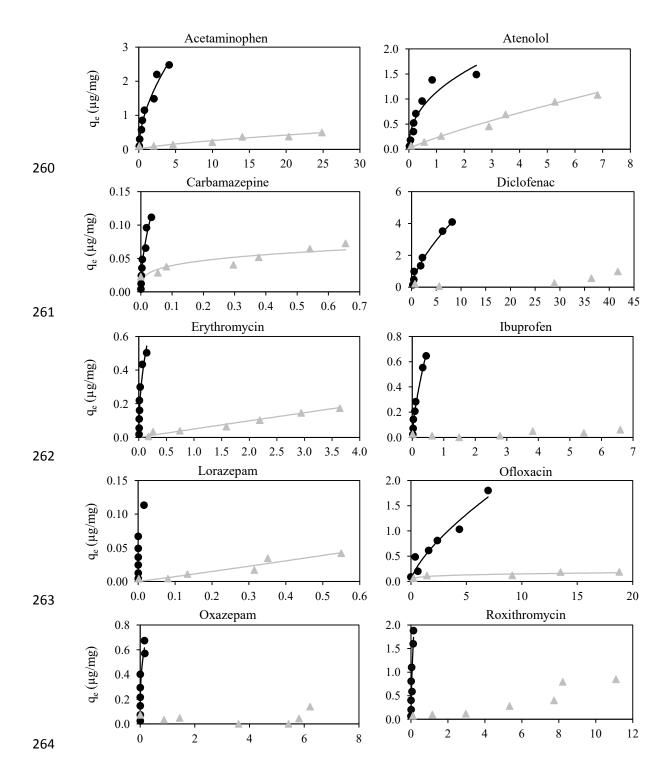
Takács, 2004). EEMs of ultrapure water were subtracted from the sample EEMs, which were also normalized by the Raman peak of ultrapure water (excitation wavelength of 350 nm) to obtain fluorescence data in Raman units (R.U.) (Lawaetz and Stedmon, 2009). EEMs were characterized by using a set of excitation/emission wavelengths based on maximum localization of 6 specific PARAFAC components (C1-C6) that were previously obtained from wastewater samples of the Seine Centre WWTP (Goffin et al. 2018). The index C1 (275/304 nm) is related to tyrosine-like compounds, C2 (285/344 nm) to tyrosine/tryptophan-like compounds, C3 (275/378 nm) to tryptophan-like compounds, C4 (295/404 nm) to humic-like compounds from a recent biological activity and C5 (360/434 nm) and C6 (275/464 nm) to humic-like compounds.

3. Results and discussion

3.1. Adsorption pseudo-isotherms

Pseudo-isotherms representing the short-term (30 min) adsorption capacity of OMPs in each matrix are presented in Figure 1 and the best-fit isotherms parameters are summarized in Table 2 (experiment 1). Most pseudo-isotherms were correctly fitted with the Freundlich equation (Student-test, p-value < 0.05 for the estimated K_F or 1/n). In ultra-pure water, only lorazepam could not be fitted by the Freundlich equation because no residual concentration was detected in most bottles after 30 min of contact time. In wastewater effluent, diclofenac, ibuprofen, oxazepam and roxithromycin were not correctly fitted (p-value > 0.05 for the estimated K_F or 1/n) and their Freundlich parameters were therefore not reported in Table 2. As expected, the adsorption capacity (i.e. q_t value for a given initial concentration) was systematically higher in ultra-pure water than in wastewater effluent for all OMPs, and all Freundlich constants (K_F) obtained after fitting the data were higher in ultra-pure water than in wastewater effluent accordingly. For most OMPs, the Freundlich intensity parameter (1/n)

was also higher in wastewater effluent than in ultra-pure water, which shows that the presence of DOM makes adsorption less favorable. The Freundlich intensity parameter was lower in wastewater effluent than in ultra-pure water only for carbamazepine and ofloxacin. This could be due to modelling issues because of analytical errors at some concentrations, leading to shifted points on the isotherm (C_t and q_t values).



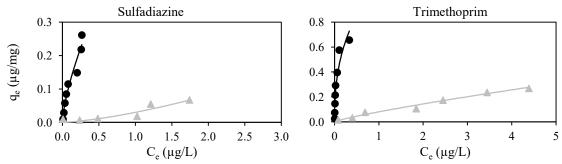


Figure 1. OMPs adsorption pseudo-isotherms after 30 min of contact time with PAC and a pre-equilibrium of 24 h between the matrix and OMPs before adsorption (experiment 1). • Ultra-pure water. A Wastewater effluent. Lines correspond to the best-fit obtained by the Freundlich model.

Table 2. Best-fit isotherms parameters of OMPs adsorption after 30 min of contact time with PAC and a pre-equilibrium of 24 h between the matrix and OMPs before adsorption (Freundlich constant K_F , intensity parameter 1/n and coefficient of determination R^2 of the model) (experiment 1). *p-values* from the Student-test are given for each parameter.

Compound	Matrix	Freundlich				
		$K_F (\mu g/mg)/(\mu g/L)^{1/n}$	p-value	1/n	p-value	R ²
Acetaminophen	Ultra-pure water	1.16	< 0.001	0.56	< 0.001	0.96
	Wastewater effluent	0.05	0.042	0.71	0.003	0.96
Atenolol	Ultra-pure water	1.14	< 0.001	0.43	0.001	0.88
	Wastewater effluent	0.23	< 0.001	0.83	< 0.001	0.98
Carbamazepine	Ultra-pure water	0.67	0.006	0.52	< 0.001	0.96
•	Wastewater effluent	0.07	< 0.001	0.25	0.048	0.72
Diclofenac	Ultra-pure water	1.00	< 0.001	0.67	< 0.001	0.98
	Wastewater effluent	-	-	-	-	-
Erythromycin	Ultra-pure water	1.38	0.006	0.48	0.001	0.88
	Wastewater effluent	0.05	< 0.001	0.98	< 0.001	0.97
Ibuprofen	Ultra-pure water	1.17	< 0.001	0.70	< 0.001	0.99
	Wastewater effluent	-	-	-	-	-
Lorazepam	Ultra-pure water	-	-	-	-	-
-	Wastewater effluent	0.08	0.017	1.05	0.019	0.92
Ofloxacin	Ultra-pure water	0.43	0.010	0.70	0.006	0.95
	Wastewater effluent	0.09	0.010	0.22	0.047	0.96
Oxazepam	Ultra-pure water	1.13	0.012	0.33	0.012	0.71
-	Wastewater effluent	-	-	-	-	-
Roxithromycin	Ultra-pure water	6.08	0.040	0.64	0.007	0.83
•	Wastewater effluent	-	-	-	-	-
Sulfadiazine	Ultra-pure water	0.58	0.002	0.69	< 0.001	0.94
	Wastewater effluent	0.03	0.010	1.44	0.039	0.88
Trimethoprim	Ultra-pure water	0.13	< 0.001	0.40	< 0.001	0.90
	Wastewater effluent	0.08	< 0.001	0.84	< 0.001	0.98

The adsorption isotherm is favorable when 1/n < 1, which suggests a good affinity between the adsorbate and the adsorbent (i.e. chemisorption), while it is unfavorable when 1/n > 1, the first adsorbate molecules are hardly adsorbed but improve the adsorption of the

following, probably through multilayer adsorption favorized by van der Waals interactions (i.e. physisorption). The adsorption of sulfadiazine was unfavorable (I/n = 1.44) and the adsorption of erythromycin and lorazepam was almost linear (I/n = 0.98 and 1.05, respectively). Erythromycin is positively charged and one of the largest molecules (MW > 700 g/mol) and could be more impacted by the presence of DOM (i.e., by pore blockage and steric hindrance).

Attractive electrostatic interactions with the negatively charged DOM were probably not sufficient to counterbalance pore blockage. Sulfadiazine is negatively charged and thus was probably subjected to repulsive electrostatic interactions with the adsorbed DOM, as well as diclofenac and ibuprofen. No correlation was obtained between Freundlich parameters and any physico-chemical property of the 12 OMPs (Table 1 and Table S2), suggesting that the adsorption of OMPs depends on various mechanisms and parameters governing their affinity with the PAC, and also their interactions with the DOM both present in solution and adsorbed at the surface of the activated carbon.

3.2. Influence of the contact time with PAC

3.2.1 DOM adsorption

DOC removal was low (4%) after 30 min of adsorption and close to values obtained in a previous study (Mailler et al., 2016b) (Table 3, experiment 2). The DOC removal was higher after 72 h (15%) but was still low despite a longer contact time. LC-OCD analyses (see Figure 2) showed that the wastewater effluent DOM was mainly composed of humic-like substances (2.58 mgC/L), followed by biopolymers, building blocks and low molecular weight neutrals (1.26-1.38 mgC/L) and to a lesser extent of hydrophobic molecules (0.75 mgC/L). Only biopolymers (especially the smallest biopolymers eluted at 33-40 min of retention time) were significantly removed after 30 min of adsorption (11 %), while almost

no removal (< 3%) was observed for humic acids, building blocks and low molecular weight neutrals. The hydrophobic fraction, which is the remaining fraction of DOC retained on the chromatographic column and not eluted, reached similar removal as biopolymers (8 %). These results show that only specific DOM fractions are adsorbed and are thus responsible for the mechanisms preventing OMPs adsorption and occurring at the surface of the AC (i.e. competition for adsorption sites and pore blockage). The removal of most DOM fractions increased after a 72 h contact time with PAC. The most adsorbed fractions were again biopolymers (34%) and hydrophobic molecules (32%), followed by building blocks (10%) and low molecular weight neutrals (14%). However, humic acids were still not removed (2%) despite being the main DOM fraction. The LC-OCD effluent profile shows a much lower proportion of humic-like substances compared to a natural water (Schulz et al., 2017) and conventional wastewater profile (Zietzschmann et al., 2014) and humic acid adsorption was more important in these two studies. The lower adsorption in this study could be due to the presence of biopolymers, unlike the other studies, which are much larger and could hinder the diffusion of humic acids to the adsorption sites. The difference in PAC used could also explain the observed differences for the adsorption of humic acids, particularly the point of zero charge.

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Table 3. DOC, DOM fractions from LC-OCD, UV_{254} and fluorescence indexes removal after adsorption for 30 min and 72 h (PAC, 10 mg/L) (experiment 2).

Dissolved organic matter fraction	Wastewater	Removal (%)	
Dissolved organic matter fraction	effluent level	30 min	72 h
DOC	7.31 mgC/L	4	15
Biopolymers	1.35 mgC/L	11	34
Humic acids	2.58 mgC/L	2	2
Building blocks	1.26 mgC/L	0	10
LMW neutrals	1.38 mgC/L	3	14
Hydrophobic fraction	0.75 mgC/L	8	32
UV_{254}	0.167 1/cm	12	24
C1 – Tyrosine-like compounds	0.59 R.U.	18	44
C2 – Tyrosine/tryptophan-like compounds	1.40 R.U.	18	46
C3 – Tryptophan-like compounds	1.35 R.U.	16	39
C4 – Humic-like compounds from a recent biological activity	1.36 R.U.	15	34

C5 – Humic-like compounds	1.77 R.U.	18	41
C6 – Humic-like compounds	1.27 R.U.	6	35

A removal of 12% was obtained for UV_{254} after 30 min of adsorption, while the intensity of fluorescence indexes was slightly more affected (15-18%) except for the index C6 (6%). After 72 h of adsorption, the decrease in UV_{254} intensity (24%) and fluorescence indexes (34-46%) was in agreement with the higher removal of DOM observed from DOC and LC-OCD measurements. However, at both contact time, the decrease in UV_{254} intensity and fluorescence indexes was proportionally higher than the removal of DOC and DOM fractions. Especially, 3 fluorescence indexes related to humic substances (i.e., C4, C5, C6) exhibited a decrease higher than 30% after 72h of adsorption while only 2% of humic acids as analyzed by LC-OCD were removed. Fluorescing molecules represent a very small portion of the DOM (Wünsch et al., 2015) and these results indicate that they were preferentially adsorbed as compared to the bulk of humic substances.

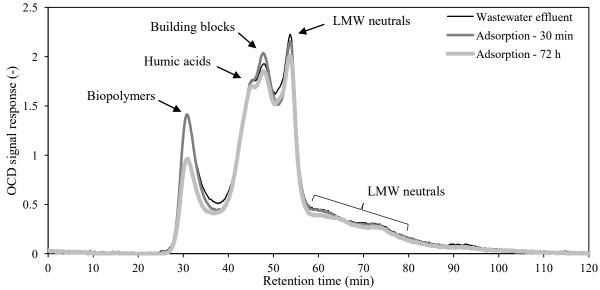


Figure 2. LC-OCD chromatograms of wastewater effluent before and after adsorption for 30 min and 72 h (PAC, 10 mg/L) (experiment 2) with fraction indicators (Huber et al., 2011). LMW: low molecular weight.

3.2.2. OMPs removal

The removal of OMPs by activated carbon was determined after 30 min and 72 h of contact time in ultra-pure water and wastewater effluent (Table 4, experiment 2). In ultra-pure water,

removals were important (> 94%) and similar between 30 min and 72 h (less than 6% difference) for almost all OMPs with the exception of diclofenac (89 and 97% at 30 min and 72 h, respectively) and ofloxacin (77 and 91%, respectively). Diclofenac and ofloxacin being negatively charged compounds, their lower removal at 30 min was possibly due to repulsive electrostatic interactions with the negatively charged PAC (pH_{pzc} = 5.0). However, ibuprofen and sulfadiazine are also negatively charged molecules but their removal was not affected, which suggests that other mechanisms favored their adsorption. Ofloxacin has a higher MW than ibuprofen and sulfadiazine, and diclofenac comprises large chlorine atoms, so differences in the diffusion rates into the activated carbon pores due to both repulsive interactions and steric hindrance effects may explain the various removals obtained for these negatively charged compounds.

Table 4. Removal of pharmaceuticals by adsorption onto PAC (10 mg/L) in ultra-pure water and wastewater effluent after 30 min and 72 h of contact time (experiment 2). A pre-equilibrium of 24 h between the matrix and OMPs before adsorption was realized. *: removal calculated using LOQ/2 as OMP concentration after adsorption.

	Removal (%)				
Compound	Ultra-pure water		Wastewater effluent		
	30 min	72 h	30 min	72 h	
Acetaminophen	94	99*	17	57	
Atenolol	96	99*	60	88	
Carbamazepine	99	99	57	99*	
Diclofenac	89	97	9	27	
Erythromycin	99	99	27	99	
Ibuprofen	96	99	4	24	
Lorazepam	99*	99*	34	73	
Ofloxacin	77	91	11	86	
Oxazepam	99*	99*	7	57	
Roxithromycin	99	99	33	99	
Sulfadiazine	94	99*	15	31	
Trimethoprim	99	99*	36	89	

In the wastewater effluent and after 30 min, removals were low (< 40%) except for atenolol and carbamazepine (60 and 57%, respectively). These low removals could be attributed to pore blockage and competition for adsorption sites caused by the presence of DOM. Biopolymers, consisting of very large molecules (> 10 kDa), were the main DOM fraction adsorbed onto PAC and thus are potentially responsible for the pore blockage. The

hydrophobic fraction of DOM, which was also better adsorbed onto PAC and can be considered in the case of wastewater as a mixture of lipids, fatty acids and lipopolysaccharides of various sizes, could also be responsible of pore blockage but also competition for adsorption sites. The positively charged and the neutral compounds were better removed than the negatively charged compounds (average removal of 40, 30 and 10%, respectively). As already observed in ultra-pure water, the occurrence of repulsive interactions between anionic OMPs and the negatively-charged PAC surface can explain these results, and these interactions can be intensified by the negatively-charged DOM adsorbed onto PAC. Conversely, the better adsorption of atenolol (presenting a positive charge at the pH of the wastewater effluent) could be attributed to attractive electrostatic interactions with the negatively charged PAC surface and the adsorbed DOM. Erythromycin and roxithromycin were again poorly removed because of steric hindrance with the DOM adsorbed in the PAC pores. After 72 h, the removal of all OMPs increased and the highest removals (ranging from 86 to 99%) were achieved for atenolol, carbamazepine, erythromycin, ofloxacin, roxithromycin and trimethoprim, which indicates that, as expected, 30 min of contact time was not sufficient to reach the equilibrium. The difference between adsorption rates at 30 min and 72 h suggests that, for these 6 compounds, the negative effect of DOM was negligible and that the adsorbed fractions of DOM (which should exacerbate higher pore blockage and competition for adsorption sites) did not prevent their adsorption in the long term. The access to adsorption sites was thus not totally prevented by DOM and no competition inside the pores occurred in the long term. Another possible mechanism is the formation of DOM-OMPs complexes that are progressively adsorbed onto the PAC surface. Pore blockage was thus the main negative effect of DOM inhibiting the adsorption of these OMPs at 30 min,

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which was finally counterbalanced by their slow diffusion either through the adsorbed DOM

or inside PAC pores. The removal of the 6 other OMPs was lower, which indicates that DOM still had a negative effect on their adsorption, either by pore blockage, competition for adsorption sites, or electrostatic repulsion from DOM moieties. The positively charged and the neutral compounds were better removed than the negatively charged compounds (average removal of 95, 75 and 42%, respectively). Erythromycin and roxithromycin were well removed despite their size, probably because of attractive interactions with both the adsorbed DOM and the PAC rather than diffusion into the PAC pores. On the contrary, low removals (ranging from 24 to 31%) were still observed for the negatively charged compounds (diclofenac, ibuprofen and sulfadiazine) and may be attributed to repulsive electrostatic interactions with both the adsorbed DOM and the PAC in addition to competition for adsorption sites. Even after a longer contact time, the presence of DOM had a higher negative effect on the adsorption of negatively charged compounds. Despite its predominant negative charge, ofloxacin was well removed in the presence of DOM (86% after 72 h) and it could be due to interactions with DOM favored by its high polar surface and number of possible hydrogen bonds in comparison to other negative OMPs. No trend was observed between the physical and chemical properties of neutral pharmaceuticals and their removals after 30 min and 72 h.

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3.3. Influence of the pre-equilibrium between DOM and OMPs on adsorption

The removal of OMPs by adsorption onto PAC for 30 min and 72 h was examined with and without a pre-equilibrium time of 24 h between the wastewater effluent and OMPs (Table 5) (experiment 3). The 24 h pre-equilibrium between DOM and OMPs increased the removal of all OMPs after 30 min of adsorption. The increase was particularly high for lorazepam (+38%) but also acetaminophen (+26%), diclofenac (+27%) and roxithromycin (+22%), which were poorly or not removed without precontact with DOM (0-11%). A significant increase was observed for atenolol (+15%), erythromycin (+15%), ibuprofen (+13%),

oxazepam (+18%), sulfadiazine (+13%) and trimethoprim (+14%). These OMPs were also poorly removed without a pre-equilibrium with DOM (4-23%) except atenolol (34%) and trimethoprim (45%). However, the pre-equilibrium with DOM had little impact on the removal of carbamazepine (+7%) and ofloxacin (+8%) which were already well adsorbed without a pre-equilibrium with DOM (41 and 47 %, respectively). Those results confirm that OMPs and DOM interacted in solution. Such association between OMPs and DOM (through hydrophobic, hydrogen bonding, van der Waals or dipole-dipole interactions) has been extensively studied, especially with natural organic matter (Caupos et al., 2015; Hernandez-Ruiz et al., 2012; Mott, 2002). Its influence on the adsorption of OMPs, specifically onto activated carbon, is however scarcely documented. Some studies demonstrated that DOM prevent the adsorption of organic compounds on river or wastewater particles but this effect could not be attributed to either DOM-OMP association in solution or to competitive adsorption (Hassett and Anderson, 1982). The co-adsorption of DOM and hydrophobic organic compounds has been reported at the surface of mineral materials (e.g. clay, kaolinite) and found to be enhanced by ionic strength (i.e. the presence of divalent cations) (Brunk et al., 1996; Wu et al., 2011). One study reported the enhanced adsorption of pentachlorophenol by PAC after a 3-day pre-equilibrium with fulvic acids, which was attributed to binding at the surface of PAC or to the modification of PAC surface properties by fulvic acid adsorption (Lafrance et al., 1991). Our results demonstrate that the DOM-OMP complexes formed after some pre-equilibration time could be subsequently adsorbed onto the PAC. The pre-equilibrium with DOM thus balances the negative effects caused by DOM presence. Further investigations would be needed to determine the potential role of inorganic ions present in wastewater effluents on the formation of these DOM-OMP complexes and their adsorption.

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The precontact of 24 h between DOM and OMPs had no impact on the removal of most OMPs after 72 h of adsorption. An increase was only observed for ibuprofen (+28%) and sulfadiazine (+36%) and in a lesser extent for lorazepam (+9%) and roxithromycine (+8%). The removal of these 4 OMPs after 72 h of adsorption and without a precontact with DOM was low (16-68%) in comparison to the other OMPs (77-98%), which didn't need interactions with DOM to be well adsorbed.

These results suggest that the precontact time between DOM and OMPs occurring during sewer transfer and inside WWTPs, therefore the processes used for primary and biological treatment, could have an impact on OMPs removal by activated carbon adsorption. DOM-OMPs complexes could also be formed at the surface of the PAC after long contact times, allowing the high removals obtained after 72h even without the 24h pre-equilibrium. These results also imply that a pre-equilibrium time between DOM and OMPs may be necessary in laboratory experiments when OMPs are spiked (e.g. adsorption isotherms) in order to have similar DOM-OMPs interactions to what can be expected in wastewater effluents.

Table 5. Removal of pharmaceuticals (initial concentration range: 0.04- $1.7 \mu g/L$, Table S2) by adsorption onto PAC (10 mg/L) with or without a pre-equilibrium time of 24 h between wastewater effluent and OMPs after 30 min and 72 h of contact time (experiment 3).

	Removal (%)				
Compound	Without 24 h precontact		With 24 h precontact		
	30 min	72 h	30 min	72 h	
Acetaminophen	9	89	35	90	
Atenolol	34	91	49	92	
Carbamazepine	41	93	48	95	
Diclofenac	11	77	38	80	
Erythromycin	20	79	35	83	
Ibuprofen	4	36	17	64	
Lorazepam	2	59	40	68	
Ofloxacin	47	98	55	98	
Oxazepam	23	86	41	88	
Roxithromycin	0	68	22	76	
Sulfadiazine	6	16	19	52	
Trimethoprim	45	96	59	98	

4. Conclusion

Adsorption pseudo-isotherms showed, as expected, that OMPs adsorption was higher
in ultra-pure water than in wastewater effluent due to the presence of DOM leading to
pore blockage and competition for adsorption sites. Various molecular properties
(e.g. charge, MW, solubility, hydrophobicity) are involved in the adsorption
mechanisms of OMPs, leading to differences in the adsorption capacity of different
OMPs.

- LC-OCD analysis revealed that biopolymers and hydrophobic molecules were the two major fractions of DOM adsorbed on the PAC (~ 30% after 72h). Other fractions were adsorbed after a contact time of 72 h (~ 10%) except humic acids despite being the main DOM fraction. The removal of DOM as analyzed by UV₂₅₄ and fluorescence indexes was higher than the removal calculated from LC-OCD analyses, which could be explained by different adsorption behaviors between the spectroscopically active DOM and the non-active one.
 - The presence of DOM had a negative impact on the removal of all OMPs after 30 min of adsorption, but similar removals to ultra-pure water were obtained after a contact time of 72 h for 6 OMPs. A sufficient contact time was thus able to allow high removals of these OMPs despite an increase of DOM adsorption, either by slow diffusion of OMPs through the adsorbed DOM or the PAC pores. Another possible mechanism is the formation of DOM-OMPs complexes that are progressively adsorbed at the PAC surface. Competition for adsorption sites is thus not always the main negative effect in the presence of DOM. Pore blockage, due to the adsorption of biopolymers, hydrophobic molecules of DOM, first strongly prevents the adsorption of OMPs, but is compensated at longer contact times by the potential mechanisms described above.

- OMPs charge had an impact on their adsorption both in the presence and absence of DOM. The adsorption rate of negatively charged compounds in the presence of wastewater effluent was reduced due to repulsive electrostatic interactions with the adsorbed DOM and the PAC surface (i.e. both negatively charged). Positively charged compounds were globally better adsorbed, possibly due to attractive electrostatic interactions, but steric hindrance hindered the adsorption rate of some large molecules.
- A pre-equilibrium of 24 h between OMPs and DOM improved their removal onto PAC, which confirm that OMPs and DOM interact in solution. These results are in accordance with the formation of DOM-OMPs complexes in solution which increased the overall removal of OMPs, especially at short contact times.
- Additional studies should be conducted to identify the nature of the interactions between DOM and OMPs, to determine the influence of various pre-equilibrium times (i.e. a kinetic study) between DOM and OMPs and optimal conditions of pre-equilibrium and adsorption contact times, as well as the influence of DOM quality (i.e. wastewater from activated sludges, biofilters, membrane bioreactors) and fractions (e.g. biopolymers or hydrophobic molecules), and the potential role of inorganic ions (e.g. divalent cations).

Acknowledgments

This study has been performed within the framework of the OPUR research program. The authors would like to thank Céline Briand (SIAAP) and Martin Maréchal (LEESU) for their help in the laboratory, Barbara Giroud (ISA), the SIAAP laboratory and DOC-Labor for the chemical analyses.

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