Benefits of ozonation before activated carbon adsorption for the removal of organic micropollutants from wastewater effluents

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1 **Title**

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3 micropollutants from wastewater effluents.

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Highlights

- OMPs adsorption increased after ozonation at high specific ozone doses only

- Ozonation performances were impacted by the presence of TSS

- Low specific ozone doses allowed the removal of OMPs refractory to adsorption

- Non-reactive OMPs toward ozone were well adsorbed onto PAC

- The best combination was 0.20-0.30 $gO_3/gDOC$ and 10 mg/L PAC

Graphical abstract
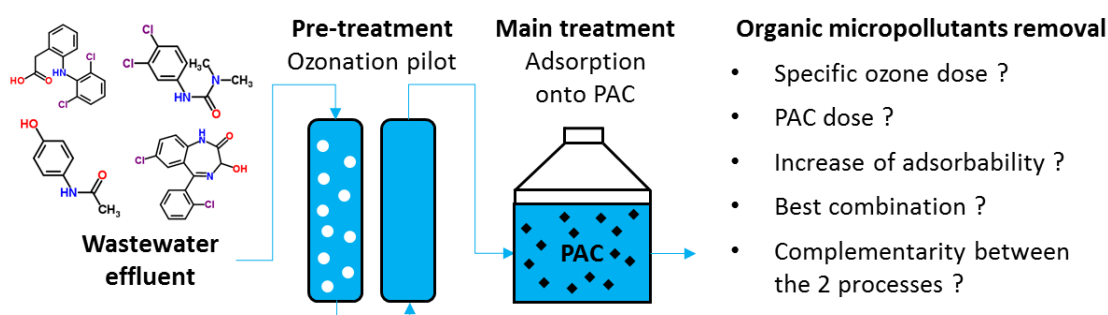
Abstract

Advanced processes for the removal of organic micropollutants (OMPs) from wastewater effluents include adsorption onto activated carbon, ozonation, or a combination of both processes. The removal of 28 OMPs present in a real wastewater effluent was studied by ozonation coupled to activated carbon adsorption and compared to a sole adsorption. The influence of the specific ozone dose (0.09-1.29 $gO_3/gDOC$) and the influence of the powdered activated carbon (PAC) dose (2, 5 and 10 mg/L) were first studied separately. OMPs removal increased with both the specific ozone dose (up to 80% for a dose higher than 0.60 $gO_3/gDOC$) and the PAC dose. Ozonation performances decreased in presence of suspended solids, which were converted to dissolved organic carbon. A correction of the specific ozone dose according to the suspended solids levels, in addition to nitrite, should be considered. The influence of ozonation (0.09, 0.22,

2

40   0.94 and 1.29 $gO_3/gDOC$) on OMPs adsorption was then assessed. OMPs adsorption didn't

41   change at low specific ozone doses but increased at higher specific ozone doses due to a decrease

42   in DOM adsorption and competition with OMPs. At low ozone doses followed by adsorption (0.22

43   $gO_3/gDOC$ and 10 mg/L PAC), the two processes appeared complementary as OMPs with a low

44   reactivity toward ozone were well absorbed onto PAC while most OMPs refractory to adsorption

45   were well eliminated by ozone. Improved removals were obtained for all compounds with these

46   selected doses, reaching more than 80% removal for most OMPs while limiting the formation of

47   bromate ion.

48   **Keywords**

49   Wastewater advanced treatment; Organic micropollutants; Ozonation; Activated carbon

50   adsorption.

51   **1. Introduction**

52   Activated carbon adsorption is widely used for drinking water production and is transferred to

53   wastewater advanced treatment to remove organic micropollutants (OMPs) and particularly

54   pharmaceuticals compounds that are refractory to biological treatments before reuse or discharge

55   in aquatic ecosystems (Altmann et al., 2015b; Guillossou et al., 2019; Meinel et al., 2015; Ruel et

56   al., 2011). Diverse types of activated carbon with different granulometries can be used, either

57   powdered activated carbon (PAC) (Altmann et al., 2015a; Kårelid et al., 2017; Meinel et al., 2016),

58   micro-grain activated carbon (µGAC) (Alves et al., 2018; Mailler et al., 2016a) or granular

59   activated carbon (GAC) (Benstoem et al., 2017; Grover et al., 2011; Zietzschmann et al., 2016).

60   The use of µGAC in fluidized bed was previously demonstrated to reach similar removals of

61   OMPs to PAC (~80-90%) (Mailler et al., 2015, 2016a) with a simpler and easier operation. However,

62   some pharmaceuticals such as diclofenac, erythromycin or sulfamethoxazole were poorly

63   removed (< 50%) by fluidized-bed µGAC, due to specific physico-chemical properties decreasing

64 their adsorption (e.g. size, charge, hydrophobicity). The presence of dissolved organic matter

65 (DOM) in wastewater effluents also limits OMPs removal through competition for adsorption

66 sites and pore blockage (Newcombe et al., 2002; Zietzschmann et al., 2014).

67 Ozonation is currently the most used oxidation process for OMPs removal in drinking water

68 production and is also recently transferred to the advanced treatment of wastewater effluents (de

69 Wilt et al., 2018; Hollender et al., 2009; Margot et al., 2013; Zimmermann et al., 2011). Bourgin

70 et al. (2018) obtained removals higher than 80 % for the 12 OMPs used as indicator substances in

71 the Swiss legislation (Office fédéral de l'environnement, Division Eaux, 2014) over a whole

72 wastewater treatment plant upgraded with an ozonation step (0.55 $gO_3/gDOC$). Ozone is a

73 powerful oxidant which reacts rapidly with electron-rich moieties such as alkenes, amines and

74 aromatic rings (von Gunten, 2003a). The self-decomposition of ozone forms hydroxyl radicals

75 ($^{\bullet}OH$) which can react with non-activated aromatic compounds, amides and alkanes. DOM and

76 OMPs are usually not mineralized but rather transformed into smaller compounds called ozonation

77 transformation products which are most of the time more biodegradable and less toxic (Hübner et

78 al., 2015; Völker et al., 2019). Oxidation by-products such as bromate (BrO_3^-) and N-

79 nitrosodimethylamine (NDMA), which are suspected to be human carcinogens, can however be

80 formed depending on the ozone dose applied and on the presence of precursors. BrO_3^- can be

81 produced from the reaction of ozone with bromide ion and NDMA from specific precursor

82 compounds (e.g. anthropogenic organic compounds containing dimethylamine groups) (Sgroi et

83 al., 2016; von Gunten, 2003b). An additional treatment step after ozonation such as sand filtration

84 or activated carbon filters is therefore required to reduce transformation products and oxidation

85 by-products.

86 In combination with activated carbon adsorption, ozonation appears as a complementary process

87 to remove compounds that are refractory to adsorption, as well as to oxidize DOM in order to

88 reduce the competition with OMPs onto activated carbon and then to limit the decrease of

89 activated carbon adsorption capacity over time. Indeed, Muller et al. (1996) reported that the

90 adsorption of the herbicide atrazine increased after pre-ozonation of DOM in river water. Matsui

91 et al. (1999) studied the effect of ozonation on the adsorption of DOM from peat water and

92 biological wastewater effluent and found a decreased in DOM adsorbability due to the formation

93 of weakly adsorbing compounds after ozonation. Zietzschmann et al. (2015) observed a decrease

94 in DOM adsorbability after the ozonation of a wastewater effluent due to a reduction of DOM

95 aromaticity, molecular size and hydrophobicity. This decrease led to a reduced adsorption

96 competition with OMPs and as a consequence improve the adsorption of OMPs on activated

97 carbon over time.

98 The coupling of ozonation and activated carbon is well known and already in use at full scale in

99 some wastewater treatment plants (WWTP) where ozonation is the main step for OMPs removal

100 and adsorption (mostly GAC) is an additional step for post-treatment. However, a coupled process

101 consisting of ozonation as a pre-treatment step (i.e. at lower doses than commonly employed)

102 followed by activated carbon adsorption as the main treatment step has never been considered.

103 The coupling could be an interesting option to increase the removal of OMPs refractory to

104 adsorption and for disinfection purposes while limiting the production of oxidation by-products,

105 but knowledge of its efficiency for real wastewater effluents, which are composed of a more

106 complex matrix than surface water, is limited. Moreover, available studies only investigated a

107 small number of OMPs spiked in wastewater effluents at relatively high concentrations (> 10

108 µg/L) (Zietzschmann et al., 2015). The aim of this study was to evaluate the removal of 28 OMPs

109 present in wastewater effluents by ozonation coupled to adsorption onto activated carbon as the

110 main treatment step, and to estimate the benefits provided by the coupling in comparison to

111 activated carbon adsorption alone. The influence of various specific ozone doses on OMPs

112 removal was first studied. The effect of the activated carbon dose was then evaluated with a

113 preliminary ozonated effluent. DOM evolution during ozonation and adsorption were examined

114   in parallel through UV_{254} and fluorescence excitation/emission analyses. Different combinations

115   of specific ozone doses and activated carbon doses were tested to assess the potential beneficial

116   effect of ozonation on OMPs adsorption through DOM oxidation, to evaluate the complementarity

117   between both processes toward OMPs that are refractory to ozonation or adsorption and to find

118   the most promising combination of specific ozone and PAC doses.

119   **2. Material and methods**

120   *2.1. Ozonation pilot*

121   The ozonation experiments were conducted on a pilot comprising a cylindrical stainless-steel

122   transfer column (height = 100 cm, diameter = 25 cm, volume = 56 L) and a contact column of

123   similar dimensions (Figure S1). The ozone gas was produced in a corona-discharge tube from an

124   oxygen-enriched gas stream (90% O_2) produced by an oxygen concentrator (OnyxUltra, CAIRE

125   Inc.). The gas was sent to the transfer column from a porous diffuser at the bottom at counter-

126   current flow in the transfer column. The concentration of the ozone inlet and outlet gas of the

127   transfer column was measured by an ozone gas analyser (BMT 964, BMT Messtchnik GMBH).

128   The ozone gas flow was maintained at a constant value (2 NL/min) and the concentration of ozone

129   ranged from 8 to 45 g/Nm^3. The ozonated water was sampled after the contact column for each

130   specific ozone dose in 20-L cleaned glass bottles. The water flow was maintained constant (10

131   L/min) and measured by a flowmeter. The hydraulic retention time in each column was about 5

132   min. The water pH (7.0-7.4) and temperature (20-25°C) were monitored by probes

133   (Endress+Hauser, Germany).

134   The pilot was fed continuously by nitrified water directly pumped from the second biofiltration

135   stage from the Seine-Centre WWTP (Colombes, France). The plant is operated by the Paris public

136   sanitation service (SIAAP) and treats wastewater for 800 000 inhabitants with a flow of 240 000

137   m^3/day. The treatment is composed of a pre-treatment step (screening, grit and oil removal)

138 followed by the primary treatment (physico-chemical lamellar settling for the removal of

139 suspended particles, colloids and phosphorus) and the biological treatment (3 stages of

140 biofiltration for the removal of carbon and nitrogen). After treatment, the effluent is discharged in

141 the Seine River. The ozone dose transferred in the liquid phase was normalized by the dissolved

142 organic carbon concentration (DOC) after subtraction of the ozone consumption by nitrite ion

143 (NO_2^-) (Naumov et al., 2010) to obtain the value of the parameter "specific ozone doses" used all

144 along the article.

145 $$Specific\ O_3\ dose = \frac{Transferred\ O_3\ dose - 1.04 * [NO_2^-]_{consumption}}{[DOC]}$$

146 With the specific O_3 dose in $gO_3/gDOC$, the transferred O_3 dose in $gO_3/L_{wastewater}$, $[NO_2^-]$

147 consumption in gNO_2^-/L and [DOC] before ozonation in g/L.

148 An instantaneous ozone demand (IOD) of the nitrified water in nominal conditions was evaluated

149 at 3.8 ± 0.5 mgO_3/L (DOC = 6 mgC/L, TSS < 2 mg/L, NO_2^- < 0.06 mg/L) following the method

150 developed by Roustan et al. (1998). The IOD was satisfied for specific ozone dose up to 0.7

151 $gO_3/gDOC$.

152 Apart from the water quality, the operating conditions did not change during the experiments

153 except the concentration of the ozone gas sent to the transfer column. An equilibration time of 15

154 min was allowed between the application of each specific ozone dose.

155 *2.2. Experimental plan*

156 The removal performances of 28 OMPs (19 pharmaceuticals, 6 pesticides, 2 hormones and 1

157 perfluorosulfonic acid – Table 1) were studied. A set of 5 experiments was conducted at various

158 specific ozone doses (ranging from 0.09 to 1.29 $gO_3/gDOC$) (Table 2). Nitrified water from the

159 Seine Centre WWTP was sampled on 2018-05-02, 2018-05-23, 2018-07-06, 2019-04-09 and

160 2019-08-07 (experiments 1 to 5, respectively). The quality of the wastewater effluent is generally

similar over this period of the year (Rocher et al., 2012). Experiment 1 and 2 were conducted to study the influence of the specific ozone dose. Experiment 3, 4 and 5 were performed to study the influence of the activated carbon dose, the performances of the coupled processes and the influence of ozonation on adsorption performances, respectively. For experiments involving PAC adsorption (experiments 3, 4 and 5), a µGAC (CycleCarb 305, Chemviron Carbon) was crushed and sieved to keep only particles between 50 and 63 µm to guarantee a fast adsorption. This activated carbon was chosen due to its previous use in a fluidized-bed industrial pilot (CarboPlus®, Saur) (Mailler et al., 2016a) and the chemical, physical and textural properties of this activated carbon (Table S1) were determined in a previous study (Guillossou et al., 2020). An average OMPs removal of 70% in this pilot was equivalent to 30% in batch with a similar PAC dose (10 mg/L) (Mailler et al., 2016b, 2015). Each desired PAC dose (2, 5 or 10 mg/L) was added to 10 L of nitrified or ozonated water in 20 L flasks then adsorption tests were performed under fast stirring for 30 min using a stainless-steel blades stirrer. The range of PAC doses was chosen from a previous work which reported that the removal gain obtained when increasing the PAC dose from 5 mg/L to 10 mg/L was more important than when increasing from 10 mg/L to 20 mg/L (Mailler et al., 2016b). Prior to adsorption in experiment 5, the 28 studied OMPs were spiked at a concentration of 100 ng/L to ensure their presence in the effluent after ozonation (high specific ozone doses).

184 Table 1. List of the 28 analysed OMPs, their reaction rate constant with ozone (k_{O3}), molecular weight (M_w), hydrophobicity (log D) and charge at 20-25°C and pH
185 = 7.0, and their limits of quantification (LOQ). The M_w, log D and charge were calculated using MarvinSketch (ChemAxon).

Compound	Use	k_{O3} (L.mol^{-1}.s^{-1})	Reference for k_{O3}	M_w (g/mol)	Log D	Charge	LOQ (ng/L)
Acetaminophen	Analgesic	2.6×10^6	Hamdi El Najjar et al., 2014	151.2	0.91	0	0.5
Acetamiprid	Insecticide	0.25	Cruz-Alcalde et al., 2017	222.7	1.11	0	1
Atenolol	Betablocker	2.1×10^3	Mathon et al., 2017	266.3	-2.24	+1	1
Carbamazepine	Anticonvulsive	3.0×10^5	Huber et al., 2003	236.3	2.77	0	1
Ciprofloxacin	Antibiotic	1.9×10^4	Dodd et al., 2006	331.3	-1.47	0	35
Clothianidin	Insecticide	-	-	249.7	-4.53	0	3
Diclofenac	Analgesic	1.0×10^6	Huber et al., 2003	296.2	1.26	-1	0.5
Diuron	Pesticide	1.5×10^1	Mathon et al., 2017	233.1	2.53	0	1
Erythromycin	Antibiotic	7.0×10^4	Mathon et al., 2017	734.0	1.20	+1	4
Estradiol	Hormone	$3.0. \times 10^6$	Huber et al., 2003	272.4	3.75	0	7
Estrone	Hormone	1.5×10^5	Deborde et al., 2005	270.4	4.31	0	2.5
Ibuprofen	Analgesic	9.6	Huber et al., 2003	206.8	1.69	-1	6
Imidacloprid	Insecticide	-	-	255.7	-1.95	0	2
Ketoprofen	Analgesic	0.4	Real et al., 2009	254.3	0.49	-1	1
Lorazepam	Anxiolytic	-	-	321.2	3.53	0	1.5
Naproxen	Analgesic	2.0×10^5	Huber et al., 2005	230.3	0.18	-1	2
Norfloxacin	Antibiotic	4.5×10^5	Ling et al., 2018	319.3	-1.57	0	5
Ofloxacin	Antibiotic	2.0×10^6	Márquez et al., 2013	361.4	-0.05	-1	1
Oxazepam	Anxiolytic	1.0	Lee et al., 2014	286.7	2.92	0	2
PFOS	Additive	1.0	Arias Espana et al., 2015	500.1	-4.89	-1	0.5
Propranolol	Betablocker	1.0×10^5	Mathon et al., 2017	259.3	-0.09	+1	1.5
Roxithromycin	Antibiotic	7.0×10^4	Huber et al., 2003	837.1	0.92	+1	0.5
Sulfadiazine	Antibiotic	1.0×10^5	Garoma et al., 2010	250.3	0.08	-1	1
Sulfamethoxazole	Antibiotic	2.5×10^6	Huber et al., 2003	253.3	-0.11	-1	1
Tetracycline	Antibiotic	1.9×10^6	Dodd et al., 2006	444.4	-0.57	0	22
Thiaclopride	Insecticide	-	-	254.7	2.06	0	2.5
Thiamethoxam	Insecticide	-	-	291.7	1.29	0	0.5
Trimethoprim	Antibiotic	3.0×10^5	Dodd et al., 2006	290.3	0.89	+1	2

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2.3. Analytical procedures

188 For each experiment, the concentrations of the 28 studied OMPs were analysed within 48 h

189 (Institut des Sciences Analytiques – Villeurbanne, France) by liquid chromatography coupled to

190 tandem mass spectroscopy. These micropollutants were chosen because of their frequency of

191 detection in the effluents of wastewater treatment plants in the Paris conurbation (Mailler et al.,

192 2015, 2014) or because they were molecules of recent interest (e.g. the 5 insecticides). Prior to

193 analysis, all samples were homogenized and filtered on 0.7 µm GF/F glass filters (Whatman).

194 Details of the analytical methods are described in supplementary information (Text S1) (Vulliet

195 et al., 2011). OMPs removal was calculated following the approach of Choubert et al. (2017),

196 which stated that the uncertainty of OMPs concentrations in wastewater generally ranges between

197 30% and 100% when the measured value is lower than 2.5 to 10 times the limit of quantification

198 (LOQ) of the compound. Therefore, when a compound was quantified at levels above 5 times the

199 LOQ in the nitrified water and above the LOQ after treatment, the removal was conventionally

200 calculated. When a compound concentration was above 5 times the LOQ in the nitrified water but

201 below the LOQ after treatment, the removal was estimated using LOQ/2. Removals were not

202 calculated when concentrations in the nitrified water and after treatment ranged between the LOQ

203 and 5 times the LOQ.

204 Conventional wastewater quality parameters were analyzed by the certified SIAAP laboratory:

205 total organic carbon (TOC), dissolved organic carbon (DOC), NH_4^+, NO_2^-, NO_3^- and total

206 suspended solids (TSS) (Table S2). Bromide (LOQ = 50 µg/L) and bromate (LOQ = 5 µg/L)

207 concentrations were measured for the first experiment after filtration on 0.7 µm GF/F glass filters

208 (Whatman) by ion chromatography (CARSO laboratory, Vénissieux, France).

209 Spectroscopic measurements were performed at room temperature directly after sampling and

210 filtration on 0.45 µm polyvinylidene fluoride filters (Milex®, Merck). UV_{254} was measured in a 1

211 cm quartz cuvette using a spectrophotometer (Genesys 10S UV-Vis, Thermo Scientific).

Fluorescence emission/excitation matrices (EEMs) were obtained using a spectrofluorometer (FP-8300, 150-W Xenon lamp, Jasco) with excitation wavelengths ranging from 240 nm to 450 nm at an interval of 5 nm and emission wavelengths from 250 nm to 600 nm at an interval of 2 nm. The samples were diluted with ultrapure water if the UV_{254} was higher than 0.080 1/cm to avoid inner filter effects due to adsorbing species present in the wastewater (Alberts and Takács, 2004). EEMs of ultrapure water were subtracted from the sample EEMs, which were also normalized by the Raman peak of ultrapure water (excitation wavelength of 350 nm), to obtain fluorescence data in Raman units (Lawaetz and Stedmon, 2009). A modified peak-picking approach based on a set of six fluorescence indexes (excitation/emission wavelengths) was applied on the corrected EEMs. These fluorescence indexes are based on maximum localization of 6 specific PARAFAC components (C1-C6), similarly to the studies of Murphy et al. (2011) and Sgroi et al. (2017), that were previously obtained from wastewater samples of the Seine Centre WWTP (Goffin et al. 2018). The C1 index (275/304 nm) is related to tyrosine-like compounds, C2 (285/344 nm) to tyrosine/tryptophan-like compounds, C3 (275/378 nm) to tryptophan-like compounds, C4 (295/404 nm) to humic-like compounds from a recent biological activity and C5 (360/434 nm) and C6 (275/464 nm) to humic-like compounds.

3. Results and discussion

3.1. Influence of the specific ozone dose

3.1.1. DOM removal

DOC removal globally increased with an increase of the specific ozone dose when TSS concentration was below LOQ (experiment 1): < 5, 5, 14 and 17% at 0.18, 0.32, 0.67 and 0.97 $gO_3/gDOC$, respectively. When TSS were detected (2-7 mg/L), DOC removal was negligible (i.e. < 5%) at 0.94 and 1.29 $gO_3/gDOC$ (experiment 5), and was even negative during experiment 2 with removals about -10, -25, and -14% for doses of 0.24, 0.60 and 0.90 $gO_3/gDOC$, respectively

236 (Table 2). The reaction of suspended solids (7 mg/L) with ozone during experiment 2 likely

237 converted particulate organic matter contained in TSS to DOC, as suggested by the decrease in

238 TSS concentration (from 7 to 3 mg/L) while TOC remained stable (~ 7 mgC/L). The effect of TSS

239 was also clearly observed during experiment 5 (TSS = 4 mg/L), exhibiting almost no removal of

240 DOC (< 5%) at 0.94 and 1.29 $gO_3/gDOC$, respectively, while TOC and TSS concentrations

241 decreased from 6 to ~ 4.5 mgC/L and 4 to 2 mg/L, respectively. Similar effects of suspended solids

242 on DOC removal by ozonation were observed in other studies (Jekel, 1994; Zhang et al., 2018).

243 Unlike DOC, the effective destruction of the unsaturated structures during ozonation, caused by

244 the electrophilic addition of ozone, lead to a regular UV_{254} decrease with the specific ozone dose

245 (~ 10 to ~ 50%), but no effect of the TSS concentration was noted (Table 2). The absence of

246 plateau at high ozone doses was attributed to aromatic molecules (i.e. absorbing at 254 nm) present

247 in important quantity in the nitrified water. All WWTP-specific fluorescence indexes strongly

248 reacted with ozone, exhibiting a regular loss of intensity in all regions of EEMs (Figure S2) at

249 increasing ozone doses (Table 2). The loss of intensity was > 70% for specific ozone doses from

250 0.32 $gO_3/gDOC$ and higher. At low specific ozone doses (0.18 and 0.24 $gO_3/gDOC$), tyrosine-like

251 organic compounds (C1 index) were less removed than other fluorescing DOM components, while

252 humic-like compounds (C5 index) were better removed at a dose of 0.18 $gO_3/gDOC$ than other

253 components. The high reactivity of humic-like substances would be due to their high aromaticity,

254 conferring a high electron donating capacity and hence a high extent of the ozone-reactive sites.

255 Those results suggest a different reactivity of the various DOM components at low ozone doses

256 but a high removal of all fluorescing compounds at higher doses. Fluorescing moieties can

257 therefore be considered more reactive toward ozone than the DOM moieties absorbing at 254 nm.

258

259

Table 2. DOC, TSS and NO_2^- levels in the nitrified water before ozonation and removal of DOC, UV_{254} and 6 fluorescence WWTP-specific indexes (C1-C6) obtained from PARAFAC analysis (Goffin et al. 2018) for different specific ozone doses.

Specific ozone dose (gO₃/gDOC)	Experiment	Nitrified water global parameters				Removal (%)							
		TSS (mg/L)	TOC (mgC/L)	DOC (mgC/L)	NO_2^- (mg/L)	DOC	UV_{254}	C1	C2	C3	C4	C5	C6
0.18	1	< 2	6	5.9	< 0.06	< 5	3	25	32	33	35	43	27
0.32						5	18	79	79	79	80	82	73
0.67						14	37	91	91	90	91	90	83
0.97						17	49	98	96	95	95	94	90
0.24	2	7	7.2	5.9	0.49	-10	15	25	42	45	41	43	35
0.60						-25	36	64	77	75	73	73	62
0.90						-14	49	91	91	89	87	85	77
0.24	3	< 2	5.1	4.8	< 0.06	< 5	15	34	39	37	36	44	28
0.09	4	< 2	4.6	4.5	0.26	< 5	12	-66	9	9	20	29	13
0.22						< 5	19	24	42	44	41	45	30
0.94	5	4	6.1	4.5	< 0.06	< 5	46	90	91	89	86	84	81
1.29						< 5	54	94	95	93	91	89	87

3.1.2. Bromate formation

The concentration of bromide ion in the nitrified water was 90 µg/L and did not vary significantly after ozonation at all specific ozone doses used in experiment 1 (0.18-0.97 gO₃/gDOC). No bromate ion was detected at any specific ozone doses (i.e. < 5 µg/L) despite bromide levels in the range 50-100 µg/L where bromate formation may become a problem (von Gunten, 2003b). The absence of bromate formation can be explained by the low reaction rate constant of bromide ion with ozone (160 L.mol^{-1}.s^{-1}, von Gunten, 2003b) in comparison to more reactive compounds such as DOM and OMPs. Zimmermann et al. (2011) observed bromate formation only at specific ozone doses higher than 0.90 gO₃/gDOC. The authors also observed NDMA formation at a specific ozone dose of 1.24 gO₃/gDOC and no N-nitrosomorpholine (NMOR). Contrary to bromate for which formation is mostly related to the specific ozone dose, NDMA formation rather depends on the concentrations and the conversion rate of precursors as well as matrix composition (Hollender et al., 2009). N-nitrosamines were not monitored in the study but future work will investigate their occurrence in similar conditions.
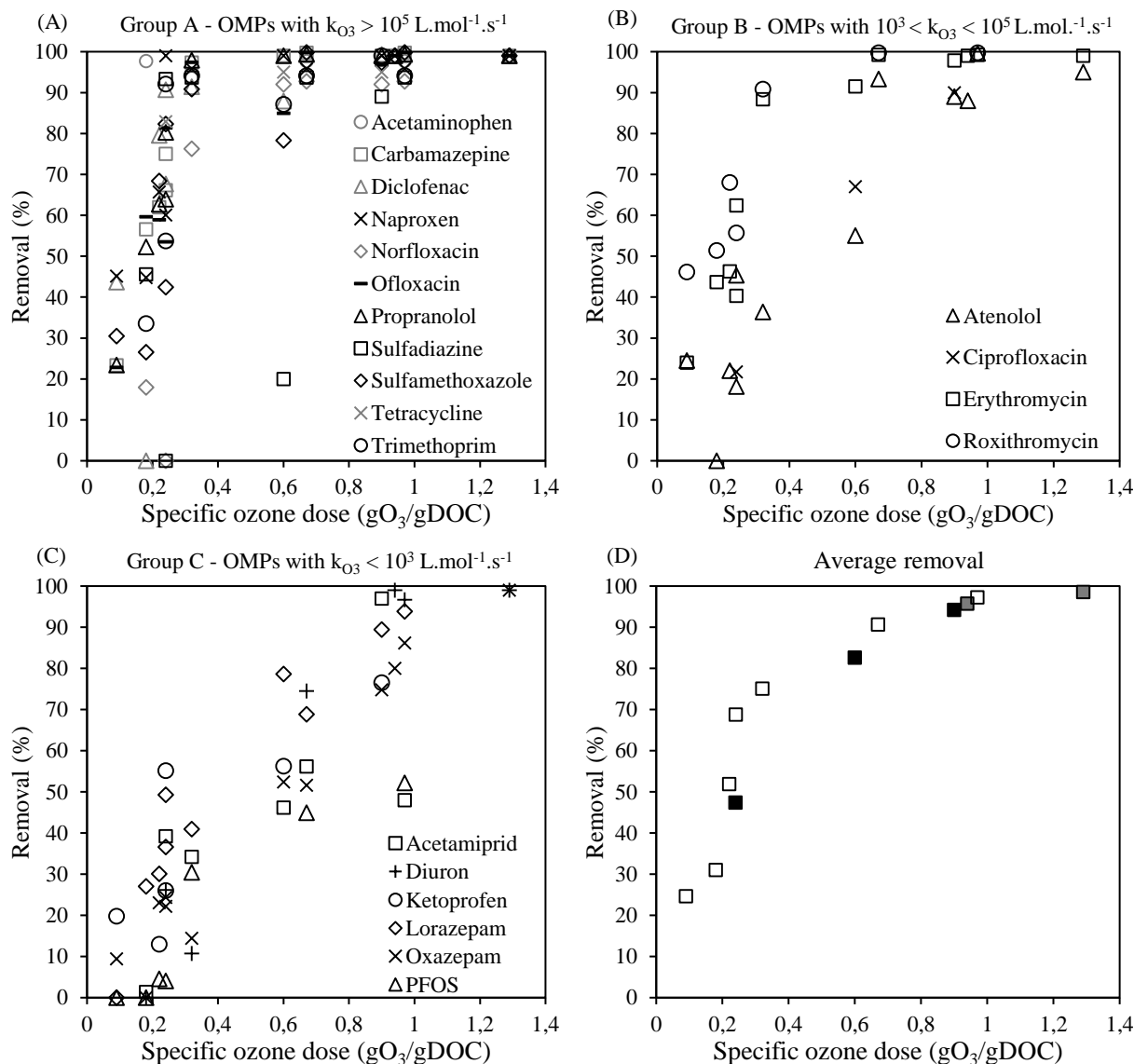
3.1.3. OMPs removal

279 Among the 28 analysed compounds, 7 OMPs were never quantified in the nitrified water

280 (clothianidin, estradiol, estrone, ibuprofen, imidacloprid, thiacloprid and thiamethoxam), 11

281 OMPs were occasionally detected (acetaminophen, acetamiprid, ciprofloxacin, diuron,

282 ketoprofen, norfloxacin, PFOS, roxithromycin, sulfadiazine, tetracycline and trimethoprim) and

283 10 OMPs were always present (atenolol, carbamazepine, diclofenac, erythromycin, lorazepam,

284 naproxen, ofloxacin, oxazepam, propranolol and sulfamethoxazole) for each experiment (Table

285 S3). Removals of the quantified OMPs were calculated at each specific ozone dose employed

286 (Figure 1). Negative removals were obtained for diuron and PFOS at low specific ozone doses (<

287 0.30 gO_3/gDOC). They were attributed to matrix effects during analyses or to the formation of

288 these molecules after ozonation of metabolites/parent molecules. However, these negative

289 removals were low (-10 to 0%) and were not subsequently considered. As proposed by Margot et

290 al. (2013), OMPs were categorized in 3 groups depending on their expected reactivity and

291 observed removals (Table S4). Group A contained 11 OMPs (acetaminophen, carbamazepine,

292 diclofenac, naproxen, norfloxacin, ofloxacin, propranolol, sulfadiazine, sulfamethoxazole,

293 tetracycline and trimethoprim) exhibiting removals higher than 80% at specific ozone doses higher

294 than 0.30 gO_3/gDOC (Figure 1.A). These results were in agreement with reaction rate constants

295 from the literature, compounds from group A being rapidly oxidized by ozone ($k_{O3} > 1 \times 10^5$ L.mol$^-$

296 ^{1}.s^{-1}).

297 4 OMPs (atenolol, ciprofloxacin, erythromycin and roxithromycin, listed as group B) were

298 supposed to react moderately with ozone (1×10^3 L.mol^{-1}.s^{-1} < k_{O3} < 1×10^5 L.mol^{-1}.s^{-1}). Atenolol

299 and ciprofloxacin did react poorly with ozone at specific doses lower than 0.50 gO_3/gDOC

300 (removals < 40%) while high removals (> 80 %) were achieved for erythromycin and

301 roxithromycin for a dose of 0.32 gO_3/gDOC, similarly to group A (Figure 1.B). Erythromycin and

302 roxithromycin have a higher ozonation constant rate (7×10^4 L.mol^{-1}.s^{-1}) than atenolol and

303 ciprofloxacin ($2x10^3$ L.mol^{-1}.s^{-1} and $2x10^4$ L.mol^{-1}.s^{-1}, respectively). A higher reactivity of

304 erythromycin and roxithromycin with hydroxyl radicals may also explain their higher removal.

305 DOM is rich in humic substances that can act either as radical scavenger or help in the formation

306 of hydroxyl radicals (Lee at al., 2013).The removal of atenolol and ciprofloxacin only reached

307 90% at specific ozone doses higher than 0.80 gO$_3$/gDOC.

308 Finally, group C comprised 4 OMPs (diuron, ketoprofen, oxazepam and PFOS) that were

309 demonstrated to be recalcitrant to ozone ($k_{O3} < 1x10^3$ L.mol^{-1}.s^{-1}) and 2 OMPs (acetamiprid and

310 lorazepam) which ozone rate constants were not found in the literature but exhibited low removals

311 (< 50% at doses < 0.5 gO3/gDOC). High specific ozone doses (> 0.90 gO$_3$/gDOC) allowed to

312 achieve high removals (> 80%) for most OMPs of group C, but low removals were still obtained

313 for acetamiprid and PFOS (48% and 52% at 0.97 gO$_3$/gDOC, respectively).

314 The average removal at each specific ozone dose was determined based on the removals of the 10

315 OMPs systematically quantified in each experiment (Figure 1.D). The average removal was low

316 (< 40%) at the lowest specific ozone doses and increased up to 90% with the higher specific dose.

317 The removal of many OMPs from groups A and B (i.e. 13 compounds) reached a plateau above

318 0.30 gO3/gDOC (> 80%). Going further this specific ozone dose only provided major gains of

319 removal for the remaining 8 OMPs (atenolol and ciprofloxacin and group C). A high variability

320 was observed at a specific ozone dose of 0.24 gO$_3$/gDOC showing average removals of 47 and 69

321 % in the presence and absence of TSS, respectively. This difference can be explained by the TSS

322 levels during experiment 2. As proposed above, ozone probably reacted with the TSS which

323 decreased the quantity of ozone available to react with OMPs. The degradation of all OMPs was

324 affected at this specific ozone doses by TSS, especially naproxen (-39%), sulfadiazine (-93%),

325 sulfamethoxazole (-40%) and trimethoprim (-38%). Such a negative effect of suspended solids on

326 OMP removal from wastewater effluents by ozonation was also reported elsewhere (Zucker et al.,

327 2015), but the reason why some molecules are more impacted than others is not yet known.

(A) Group A - OMPs with $k_{O3} > 10^5$ L.mol^{-1}.s^{-1}

(B) Group B - OMPs with $10^3 < k_{O3} < 10^5$ L.mol.$^{-1}$.s^{-1}

(C) Group C - OMPs with $k_{O3} < 10^3$ L.mol^{-1}.s^{-1}

(D) Average removal

Figure 1. Removals of the quantified OMPs (A, B and C) and average removal (D) at different specific ozone doses (white squares TSS = 2 mg/L, grey squares TSS = 4 mg/L, black squares TSS = 7 mg/L). The average removal was calculated from the removals of 10 OMPs that were systematically detected in each experiment. A table with detailed results for OMPs removal is presented in supplementary information (Table S4).

3.2. Influence of the activated carbon dose

3.2.1. DOM removal

Before adsorption, the nitrified water was ozonated at a dose of 0.24 gO$_3$/gDOC (experiment 3). The removal of DOC, UV$_{254}$ and fluorescence WWTP-specific indexes increased with the PAC dose (Table S5). At the lowest PAC dose of 2 mg/L, all removals were low and similar (0-6 %), the highest removal being attained for the C2 index related to tyrosine and tryptophan-like compounds. At a PAC dose of 5 mg/L, the C2 index exhibited again the highest removal (20%)

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342   and other removals ranged between 1 and 11%. A low removal was observed for UV_{254} with a

343   PAC dose of 10 mg/L, while the best removals were obtained for indexes C1, C2, C3 and C4 (18-

344   23%). These 4 indexes are related to small DOM fractions (aromatic proteins-like, tyrosine-like,

345   tryptophan-like and humic-like from a recent biological activity) which had probably a better

346   access to the PAC porosity in 30 min. Sgroi et al. (2018) observed a better removal of humic-like

347   fractions than tyrosine and tryptophan-like, but it is well known that that the distribution of

348   activated carbon porosity between macro-, meso- and micropores has an influence on DOM

349   adsorption (Guillossou et al., 2020; Li et al., 2003). As a result, the different type of activated

350   carbon used in this study led to a different behavior toward the adsorption of various DOM

351   fractions.

352   3.2.2. OMPs removal

353   Among the 28 compounds analyzed, 10 OMPs (acetaminophen, acetamiprid, clothianidin,

354   estradiol, ibuprofen, imidacloprid, norfloxacine, tetracycline, thiacloprid and thiamethoxam) were

355   not quantified in the ozonated water (0.24 gO_3/gDOC, experiment 3). 8 compounds (ciprofloxacin,

356   estrone, ketoprofen, lorazepam, naproxen, sulfadiazine, sulfamethoxazole and trimethoprim) were

357   quantified at concentrations close to their LOQ so their removal was not calculated. Removals of

358   the 10 remaining OMPs at the 3 different PAC doses (2, 5 and 10 mg/L) are presented in Figure

359   2.

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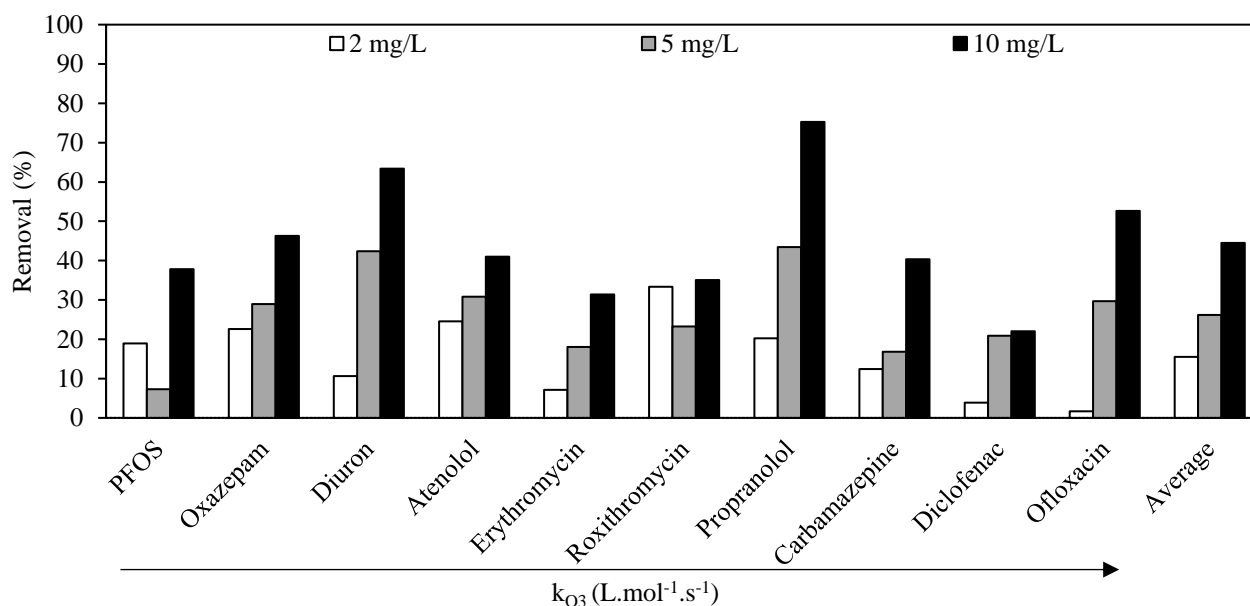
Figure 2. Removals of the 10 OMPs quantified in the ozonated effluent (0.24 gO₃/gDOC) and the average removal at 3 different PAC doses (2, 5 and 10 mg/L) after 30 min of contact time (experiment 3). OMPs are ranked with respect to their k_{O3} value (increasing from left to right).

OMPs removals were all lower than 30% at a PAC dose of 2 mg/L. At 5 mg/L of PAC, removals remained between 10 and 30% except for diuron (42%) and propranolol (43%). Those 2 compounds showed a better adsorption than other OMPs in other studies (Margot et al., 2013; Ruel et al., 2011). In a previous study using PAC, their removal was higher than 60% at a dose of 10 mg/L while those of other OMPs remained between 20 and 60% (Mailler et al., 2015). More information on the effect of the physico-chemical properties of OMPs on their adsorption can be found in a previous study (Guillossou et al., 2020). The average removal increased regularly with the dose (14, 25 and 42%). A PAC dose of 10 mg/L provided the highest removals after ozonation and was thus selected for the subsequent experiments. Notably, substantial removals (> 30%) were obtained for compounds presenting a low k_{O3} (e.g. PFOS, oxazepam, diuron) which would guarantee their removal during a coupled ozonation/adsorption process.

3.3. Influence of ozonation on adsorption performances

3.3.1. Influence of ozonation on DOM adsorption

DOC and UV removals by adsorption after ozonation at low specific doses (0.09 and 0.22 gO₃/gDOC, experiment 4) remained low (< 12%) and were not significantly different from

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380   nitrified water, while a slight increase was observed for fluorescence indexes (Table S6).

381   However, the removal of DOC, UV$_{254}$ and all fluorescence indexes by adsorption after ozonation

382   at 0.94 and 1.29 gO$_3$/gDOC (experiment 5) decreased, which suggests that DOM adsorbability

383   decreased at high specific ozone doses. These results are in accordance with the observations of

384   Zietzschmann et al. (2015) who found a decrease in DOM adsorbability at high specific ozone

385   consumptions (0.65 and 1.64 gO$_3$/gDOC) due to a reduction of DOM aromaticity, molecular size

386   and hydrophobicity.

387   3.3.2. Influence of ozonation on OMPs adsorption

388   Removals by adsorption onto PAC (10 mg/L) after ozonation at 4 different specific ozone doses

389   were obtained for the 13 OMPs quantified before adsorption (Figure 3). The average removal after

390   adsorption was similar between the nitrified water (31-36%) and the ozonated water at low

391   specific ozone doses (33 and 36% at 0.09 and 0.22 gO$_3$/gDOC, respectively, experiment 4)

392   suggesting no effect of pre-ozonation on OMP adsorption at these specific doses.

393   OMPs adsorption increased at higher specific ozone doses (experiment 5) with an average removal

394   of 52% for a dose of 0.94 gO$_3$/gDOC and 61% for a dose of 1.29 gO$_3$/gDOC, confirming the

395   positive effect of high ozone doses (> 0.50 gO$_3$/gDOC) on the subsequent adsorption, as

396   previously suggested by Zietzschmann et al. (2015). The decrease in DOM adsorbability (also

397   observed in the study, see part 3.3.1) probably involves a reduction of the competitive adsorption

398   with OMPs. Individual removals of atenolol, carbamazepine, ketoprofen, lorazepam, ofloxacin,

399   oxazepam and propranolol (Figure 3.A) followed a similar behavior to the average removal

400   (Figure 3.D). For some OMPs (diclofenac, PFOS and sulfamethoxazole), the increase of their

401   removal was only observed at the highest specific ozone dose (1.29 gO$_3$/gDOC), while ozonation

402   at any dose had no effect on the adsorption of erythromycin, naproxen and roxithromycin. The

403   adsorption of erythromycin and roxithromycin was previously demonstrated to be impacted by

404   steric hindrance because of their high molecular weight, and thus are not subject to competition

405   with DOM (Guillossou et al., 2020).

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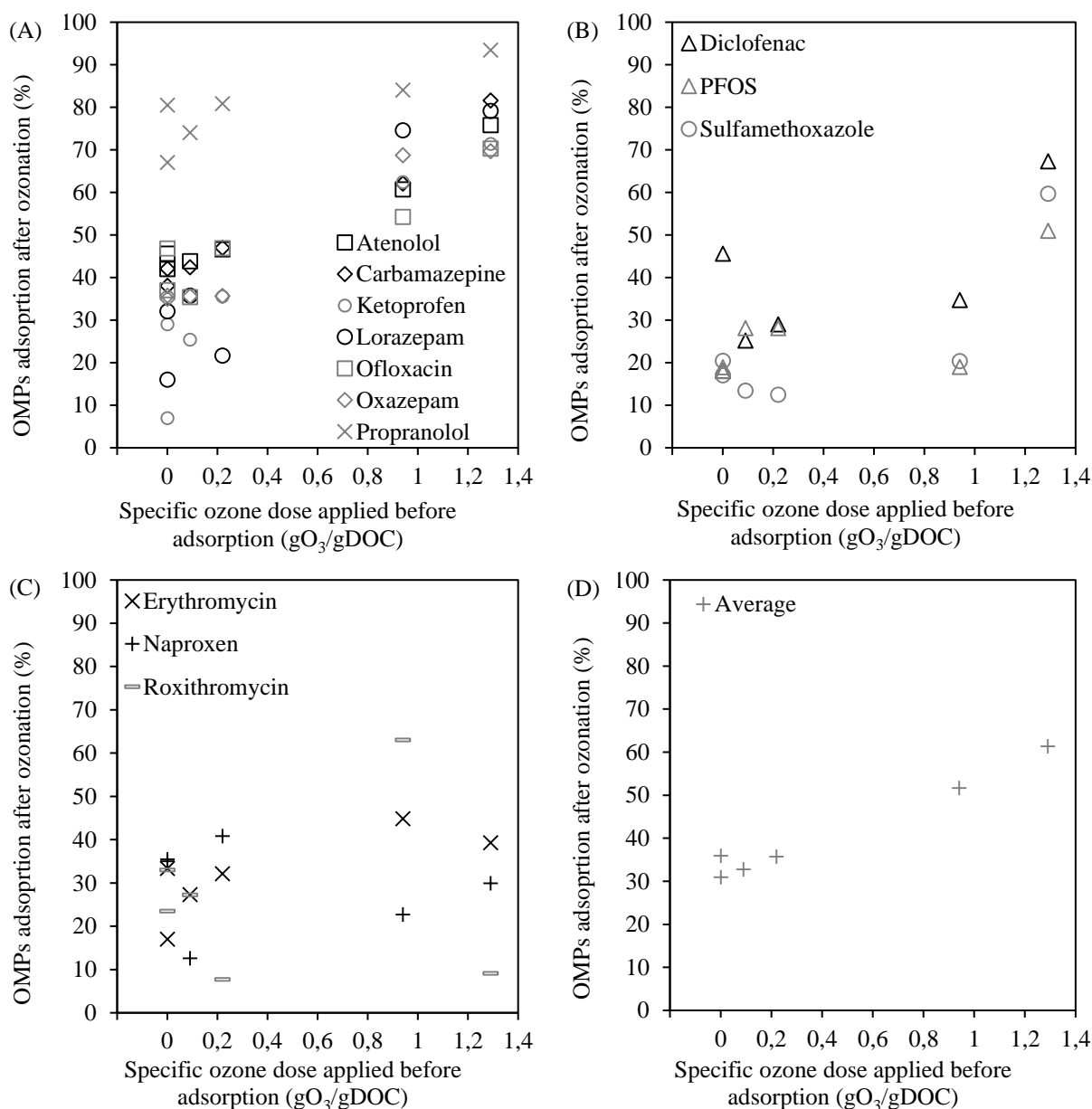
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408   Figure 3. OMPs removal by adsorption onto PAC (10 mg/L) after ozonation of the nitrified water at various
409   specific ozone doses.

410   *3.4. Comparison of coupled ozonation/adsorption with adsorption alone*

411   3.4.1. OMPs removal

412   Among the 28 analyzed compounds, 7 OMPs (acetamiprid, clothianidin, estradiol, estrone,

413   imidacloprid, thiacloprid and thiamethoxam) were not quantified in the nitrified water during

experiment 4 (Table S3). In addition, the removal of 8 OMPs (acetaminophen, ciprofloxacin, diuron, estrone, ibuprofen, norfloxacine, sulfadiazine and trimethoprim) was not calculated because their concentrations in the nitrified water were close to their respective LOQ. As expected, higher overall removals were obtained with ozonation coupled to adsorption (average removal of 49 and 66% with 0.09 and 0.22 gO_3/gDOC + 10 mg/L of PAC, respectively) than the sole adsorption (average removal of 31% with a PAC dose of 10 mg/L) (Figure 4). The highest removals were achieved when combining 0.22 gO_3/gDOC and 10 mg/L of PAC, reaching more than 80% for 4 OMPs (carbamazepine, diclofenac, naproxen and propranolol). 5 OMPs exhibited moderate removals ranging from 58 to 72% (atenolol, erythromycin, ofloxacin, roxithromycine and sulfamethoxazole) and 4 OMPs were less removed than the average with removals ranging from 31 to 50% (ketoprofen, lorazepam, oxazepam and PFOS). At higher ozone doses (0.94 and 1.29 gO_3/gDOC, experiment 5), all OMPs reached removals > 99%, except atenolol and oxazepam with 88 and 80% removal at 0.94 gO3/gDOC (data not shown on Figure 4).
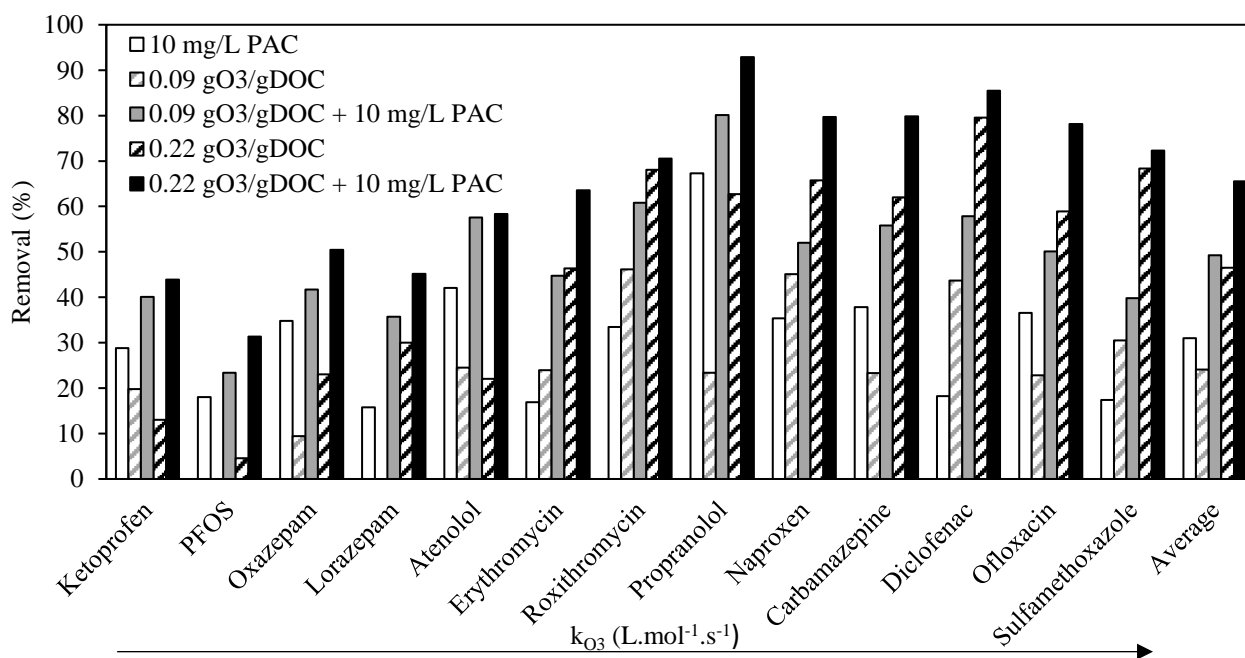
Figure 4. Removals of the 13 quantified OMPs and the average removal at different ozone and PAC doses (experiment 4). OMPs are ranked with respect to their k_{O3} value (increasing from left to right).

433   3.4.2. Complementarity of the two processes

434   As illustrated in Figure 5, a general increase in removals was provided by the coupling of

435   ozonation with adsorption, especially for molecules that were not well removed by ozonation

436   alone. After ozonation at 0.22 gO_3/gDOC (experiment 4), PAC adsorption improved the removal

437   of OMPs with low k_{O3} values (e.g. ketoprofen, oxazepam, PFOS, $k_{O3} < 10^4$ $L.mol^{-1}.s^{-1}$) with an

438   addition removal of 25% in average. OMPs with high k_{O3} values (e.g. diclofenac, naproxen,

439   ofloxacin, $k_{O3} > 10^4$ $L.mol^{-1}.s^{-1}$) exhibited an additional removal by adsorption of only 12% in

440   average. At the lower ozone dose of 0.09 gO_3/gDOC (experiment 4), overall removals of

441   compounds reacting slowly with ozone were also higher (additional removal by PAC of 28% in

442   average) as compared to the ozone-reactive OMPs (additional removal by PAC of 22% in average)

443   (Figure S3). At higher ozone doses (0.94 and 1.29 gO_3/gDOC, experiment 5), the removal of

444   OMPs by ozone was largely predominant (> 99% for almost all molecules), so the gain provided

445   by the adsorption was insignifiant (data not shown).

446   Conversely, ozonation coupled to activated carbon adsorption was also interesting for OMPs

447   exhibiting a low affinity with PAC such as diclofenac, erythromycin, lorazepam, PFOS and

448   sulfamethoxazole (Figure 6 and Figure S4). The addition of an ozonation step before adsorption

449   provided an additional removal, for OMPs refractory to adsorption (i.e. removal < 30% for the

450   sole adsorption), of 21 and 38% in average for specific ozone doses of 0.09 and 0.22 gO_3/gDOC,

451   respectively. For compounds that were better adsorbed such as atenolol, carbamazepine,

452   ketoprofen, naproxen, ofloxacin, oxazepam, propranolol and roxithromycin (removals > 30% by

453   PAC), the additional removal provided by ozonation was lower but still significant (16 and 32%

454   in average at 0.09 and 0.22 gO3/gDOC, respectively). The removal of all the quantified OMPs

455   was higher than 30% after ozonation and adsorption. These results are particularly interesting

456   because they highlight a possible optimum in the operating conditions when ozonation is

457   combined with activated carbon adsorption to treat OMPs in real wastewater effluents. In addition,

the use of activated carbon should allow the adsorption of ozonation byproducts formed during

ozonation (e.g. hydroxylated products or N-oxides) (Merel et al., 2017). Additional studies should

be conducted (e.g. by using non-targeted analyses, Schollée et al. (2018)) to study if such

transformation products can be effectively adsorbed on activated carbon.
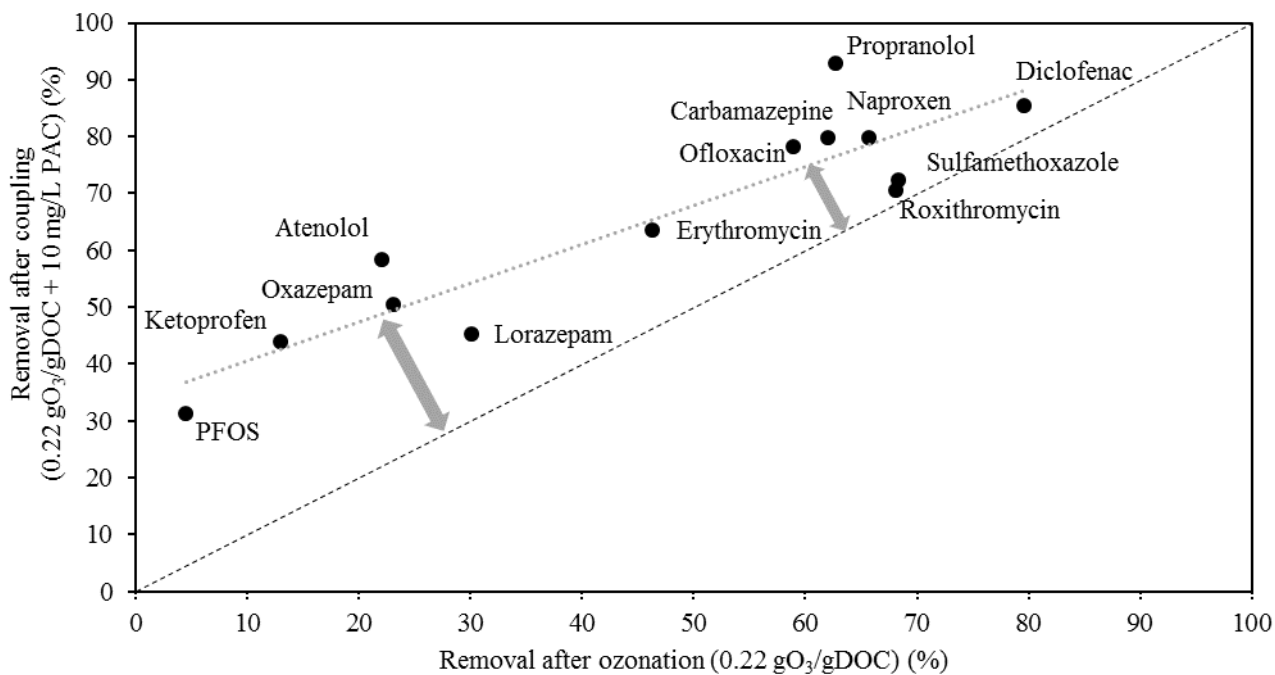
Figure 5. OMPs removal after coupling (0.22 gO_3/gDOC + 10 mg/L PAC) compared to ozonation alone (0.22 gO_3/gDOC).
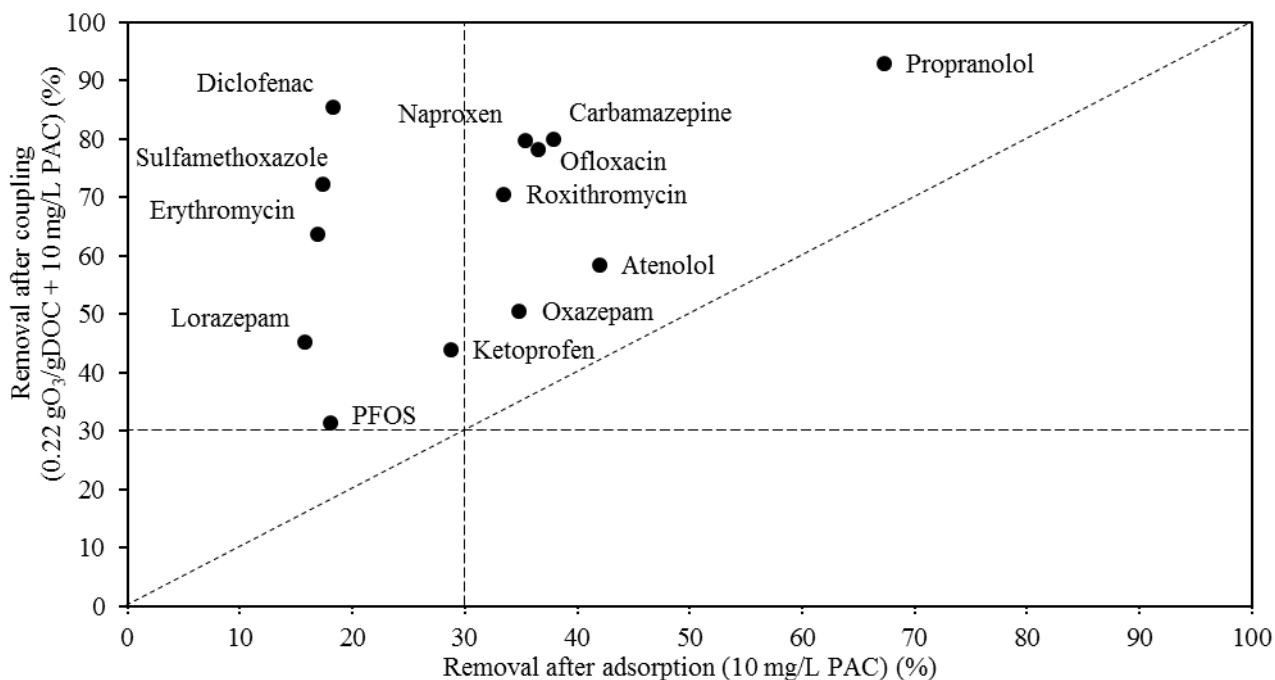
Figure 6. OMPs removal after coupling (0.22 gO_3/gDOC + 10 mg/L PAC) compared to adsorption alone (10 mg/L).

Conclusion

- Ozonation is an efficient process for OMPs elimination from wastewater effluents, with average removals higher than 80% for specific ozone doses higher than 0.60 $gO_3/gDOC$. An increase in the average removal was observed with the increase of the specific ozone dose and the removals of 13 reactive compounds reached a plateau above 0.30 $gO_3/gDOC$. Higher doses (> 0.80 $gO_3/gDOC$) were necessary for less reactive compounds.

- The ozonation performances for OMPs removal thus seemed to be dependent of the wastewater quality, especially for low specific ozone doses where a higher competition between OMPs and the matrix for ozone can be expected. Online monitoring of the quality of the matrix (DOC, TSS, NO_2^-) therefore seems interesting to achieve stable ozonation performances. Further study is needed to better understand the negative influence of TSS on ozonation performances and the conversion of TSS to DOC. A correction of the specific ozone dose according to the TSS concentration, as for nitrites, could then be considered. No bromate was detected at any specific ozone doses in this study.

- The influence of ozonation on adsorption performances was not significant at low specific ozone doses (0.09 and 0.22 $gO_3/gDOC$) but an increase in OMPs adsorption was observed at higher doses (0.94 and 1.29 $gO_3/gDOC$). This increase was attributed to the decrease in DOM adsorbability which led to a reduced adsorption competition with OMPs. Further experiments are needed to determine precisely the specific ozone dose at which the adsorbability of DOM decreases and to identify which DOM fractions are responsible for this decrease after oxidation.

- A better adsorption of OMPs that were poorly reactive toward ozone was observed as compared to the adsorption of highly ozone-reactive OMPs. Conversely, OMPs refractory to adsorption were well removed by ozonation. As a result, the removal of all OMPs were substantially improved with the addition of ozonation prior to adsorption. Even if low

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specific ozone doses did not improve OMPs adsorption in comparison to higher doses, low ozone doses coupled to activated carbon adsorption appear as complementary and an adequate process for the removal of various micropollutants in wastewater effluents. The formation and adsorption of ozonation transformation products should also be carried out to better evaluate the complementarity of the two processes. A life cycle analysis is needed to estimate the benefit of reducing ozone doses in terms of energy consumption while using a subsequent adsorption onto activated carbon as compared to a single ozonation step at higher doses coupled to adsorption or sand filtration.

- Based on the quality of the wastewater studied, a specific ozone dose of 0.20-0.30 $gO_3/gDOC$ and a PAC dose of 10 mg/L is recommended to achieve satisfactory performances for a wide range of OMPs (e.g. a removal higher than 80% for carbamazepine and diclofenac which are used as indicator substances in the Swiss regulation).

Acknowledgments

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