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Abstract

Methane hydrate is being considered as a potential future energy source but also a considerable geo-hazard. In this study, methane hydrate bearing sand sediment was firstly created by pressurizing methane gas into already chilled moistened packed sand specimen (excess gas method). The excess gas was then replaced by water at high pressure. Afterward, a heating/cooling cycle was applied under undrained conditions in order to completely dissociate gas hydrates and then recreate them inside the specimen. Finally, the pore pressure was reduced to zero to dissociate the gas hydrates. The whole process was performed in a magnetic resonance imaging (MRI) system allowing the determination of water and/or gas and hydrate quantity (and spatial distribution) at various times. The MRI signal was finally analyzed to interpret various processes in sand sediment: initial hydrate formation, heating-induced hydrate dissociation, cooling-induced hydrate re-formation, and depressurizing-induced hydrate dissociation.

Keyword: gas hydrate bearing sand sediment, dissociation/formation, kinetics, magnetic resonance imaging.

1. Introduction

Natural gas hydrates (primarily methane hydrates forming naturally at high pressures and low temperatures) are nowadays being considered as an alternative energy source [1]. Among the existing methods of gas recovery from hydrates, depressurization method is being considered as the most economically promising method [2]. This method, conducted by lowering the pressure in overlying sediments, may be hampered by the formation of ice and/or the reformation of gas hydrates (GH) because of the endothermic cooling nature of GH. Fundamental understandings of hydrate dissociation kinetics models are essential to predict hydrate reservoir dissociation process in the objective of selecting appropriate hydrate bearing zones and estimating gas production behavior before execution of any field tests. Some kinetics models were developed to simulate the production process based on heat/mass transfer and/or intrinsic kinetics of hydrate decomposition and/or gas-water two-phase flow [3,4]. Different assumptions were used, their applicability to reservoir level studies is also limited case by case. Various GH reservoir simulators (computational tools taking into account the complex highly-coupled transport equations, the reaction kinetics, the phase transition and the physical/chemical properties of hydrate bearing sediment) are being developed [5,6]. The accuracy of reservoir model needs, however, to be improved and the availability of long-term field production test data is so important. Two successful offshore field tests (together with two onshore field tests in Mount Elbert – Alaska and Malik in 2007 [7]), up to now, used the depressurization method. The first offshore methane hydrate production test was conducted by Japan Oil, Gas, and Metals National Corporation (JOGMEC) in the eastern Nankai Trough. Approximately 120,000 m³ of methane gas (20,000 m³/day) was produced by lowering pressure from 13.5 MPa to 4.5 MPa. The production was

interrupted due to an unexpected increase in sand production [8]. Recently in 2017, the China Geological Survey extracted 120,000 m³ of gas from natural gas hydrate deposits in the Shenhu area with a methane concentration of 99.5 percent (Xin Z. China wraps up combustible ice mining trial, setting world records. Xinhua. Guangzhou, 09 July 2017). As production costs are still high, an economically feasible way to exploit gas hydrate on a large scale should be found to commercialize the production of the natural gas hydrate. As it is challenging to get intact cores of methane hydrate-bearing sediments, most the experimental works concern laboratory tests on synthetic specimens to investigate hydrate dissociation rate, pressure-temperature evolution [9–13]. The experimental reactor scale is a crucial factor; a larger reactor better mimics actual field conditions but it would be more difficult to ensure the homogeneity of synthesized specimens [14].

In the objective of creating synthetic methane hydrates in sandy sediments, some methods were proposed and well-studied as: dissolved gas [15], partial water saturation [16], excess water [17] or ice-seeding [18]. Among them, dissolved gas and water excess method are supposed to form non-cementing hydrate habit in sandy sediments. However, dissolved gas is time-consuming method especially at high hydrate saturation because of low solubility of methane gas in water [15]. In addition, methane hydrate is observed form heterogeneously inside the sample by using water excess method by mean of X-Ray Micro-Tomography [19] and measures of pressure at different positions in the sample [20]. Recently, Choi et al. [21] proposed an efficient and consistent method by combining the partial water saturation, saline water injection at restricted conditions and a temperature cycle. However, V_P after the heating process

is quite high while sample is not saturated. The hydrate dissociation is perhaps not finished before the hydrate reformation.

Besides elastic wave velocity measurement [18,22–24] and synchrotron X-ray computed tomographic microscopy [25,26], which are used to study the kinetics and mechanisms of hydrate formation and dissociation, ^1H Nuclear magnetic resonance spectroscopy (NMR), in particular Magnetic Resonance Imaging (MRI) (at macroscopic scale of NMR) is a well-suited mean to quantitatively/qualitatively follow these kinetics. In most MRI studied cases, glass beads were used to simulate the porous media to investigate the tetrahydrofuran (THF), carbon dioxide (CO_2) hydrate formation and dissociation [27,28]. Methane hydrate formation (by dissolved gas or partially water saturation methods) was observed via Mean Intensity (MI) evolution and 2D images [29,30]. Effects of different sizes of glass beads on hydrate growth stage were investigated. In general, hydrate growth rate increases when the size of the porous media decreases. In addition, three growth stages of methane hydrates formed after the partially water saturation method were observed: the initial growth, the rapid growth and the steady stage. In sandstone media, methane hydrate formation and spontaneous conversion of methane to CO_2 hydrate were studied by mean of MI and 3D images [31,32]. As time is needed to take 3D images, spatial distribution of specimen during the hydrate formation was not measured regularly. The formation of methane hydrates in unconsolidated bed of silica with different size ranges was investigated by following the MI evolution, measured on vertical and horizontal slices [33]. The formation was observed non-uniform and occurred at different times and different positions. In addition, by using different water saturations, hydrate formation was found to be faster for lower water content. The methane hydrate formation,

dissociation and reformation in partially water saturated Ottawa sand at different water saturations were studied by combining measurements of M/I and elastic velocities [34]. M/I profiles along the specimen axis after these three procedures (hydrate formation, dissociation and reformation) show an almost homogenous distribution of GH. The fact of consolidating unsaturated sand makes water distributed more homogeneously before the gas hydrate formation. The effect of depressurizing range and rate on methane hydrate dissociation, in particular, the hydrate reformation and ice generation due to fast depressurizing rate were observed [35,36].

In this study, methane hydrate formation based on the method proposed by Choi et al. [21], but modified to improve the heating-cooling process and to adapt better with existing facilities is investigated in the objective of following the specimen homogeneity during the whole GH formation phase. In addition, GH dissociation after depressurization method is observed. Methodological efforts were put in getting fast enough measurements to follow the kinetics of GH formation/dissociation during transitory steps.

2. Experimental method

2.1. Materials

The soil used in this study is Fontainebleau silica sand (NE34). It consists of poorly graded sub-rounded grains having diameter ranging from 100 to 300 microns (see the grain size distribution curve in Figure 1 obtained by laser diffraction analysis). The physical characteristics of this material are detailed in Table 1. Tap water and methane gas with 99.995% of purity were used in the tests.

2.2. Experimental setup

The schematic views of experimental setup are presented in Figure 2. The sand specimen (1), 38 mm in diameter and 76 mm in height, is covered with a neoprene membrane (2). The confining pressure is applied to the specimen by a volume/pressure controller (7) using a perfluorinated oil (Galden®) as confining fluid (3), chosen due to its low signal intensity in MRI measurements. Methane gas is injected via the bottom inlet (5) by a pressure controller connected to a gas flowmeter (10). The top inlet (6) is closed in this study. A second volume/pressure controller (12) is used to control the water pore pressure. The specimen temperature is controlled by circulating a perfluorinated oil (Galden®), which is connected to a cryostat (8), around the cell (4). The cell is installed in a nuclear magnetic resonance imaging system (13) for observations.

Proton (^1H) NMR/MRI measurements are performed at a Bruker 24/80 DBX spectrometer operating at 0.5T (21MHz proton frequency) equipped with:

- A birdcage RF coil 20cm in diameter and height where the whole pressure cell can fit
- A BGA-26 gradient system delivering a maximum gradient strength of 50mT/m with a rising time of 500 μs .

Measurement protocols used in this work rely on well-established methodology. They consist of:

- A pulse acquisition sequence, where the overall NMR signal owing to hydrogen is measured after a dead time of 40 μs following the exciting RF pulse. This signal is referred to as 'FID INTENSITY' signal hereafter.

- A 1D profile imaging based on spin-echo acquisition with a read-out gradient orientated in the vertical direction and an echo time of 4.2ms, which provides profile measurements with 200 pixels covering a field of view of 20cm, being large enough to avoid any image aliasing owing to some parts of the external set-up to the observation zone. It provides a space-resolved view of the contribution

In both kinds of measurement, the signal intensity is expected to be proportional to the amount of hydrogen atoms owing to either liquid (water) or gas (methane) phases. Note that due to the Curie-law for spin polarization, the signal intensity is also inversely proportional to the absolute temperature in °K of the sample. The dead-time and the echo time are regarded as short enough to neglect bias owing to spin-spin relaxation. On the contrary, the gas-hydrate phase, and ice phase are negligible due to its short spin-spin relaxation time. Let us emphasize that FID intensities do not correspond directly to profile intensities, since the integration relationship between them depends on other parameters such as the sample size and the fluid amount out of the sample. Related data are then presented on independent scales.

If any, the related data processing relied on home-made routines under Scilab.

2.3. Test procedure

Methane hydrate bearing sediment (MHBS) specimens were prepared by the following procedure:

- Step 1 - Compaction: A determined quantity of moist sand (having known moisture content) is tamped in layers to obtain a specimen with a void ratio of 0.63 inside the neoprene membrane before the assembly of the experimental setup as shown in Figure 2.

- Step 2 - Consolidation: The confining pressure is increased to 25 MPa then decreased to 10 MPa).
- Step 3 – Hydrate creation: The temperature of the cell is decreased to 2 °C. Vacuum is then applied to eliminate pore air in the specimen prior to the injection of methane gas at 7 MPa of pressure.
- Step 4 – Water saturation: The valve V_2 is opened to atmosphere during a short period to let all the excess methane gas (initially under a pressure of 7 MPa) escape from the specimen (pore pressure decreases to zero), this valve is closed after that. Expecting that gas hydrates do not dissociate during this short period. The valve V_1 is then immediately opened, the bottom inlet is connected to the volume/pressure controller (12) to inject tap water (at ambient temperature) fixed at 7 MPa of pressure to the sample. This procedure is used to replace the excess gas in the specimen by water while minimizing the disturbance of methane hydrates that already exist inside the specimen. Gas hydrate pressure – temperature conditions are the same as that at the end of step 2. Skempton's coefficient is measured at the end of this step to make sure that the sample is fully saturated.
- Step 5 – Heating-induced hydrate dissociation: From this step, the confining pressure is imposed to be always 3 MPa higher than the pore pressure. The pore pressure is first decreased from 7 MPa to 4 MPa. The drainage valve (V_1) (V_2 is always closed) is then closed and the temperature of the cell is increased up to higher than 25 °C. This aims at heating the specimen under undrained condition to dissociate the existing gas hydrate progressively. Note that the pore pressure at the end of this step is higher for higher initial hydrate saturation. In addition, the capacity of pore pressure sensor in this study is limited at 19MPa.

The pore pressure is increased to 19 MPa at the end of this step so that this test procedure can be always feasible regardless of the hydrate saturation.

- Step 6 – Cooling-induced hydrate re-formation: The cell temperature is decreased to 2 °C while the pore pressure is maintained constant at 19 MPa by injecting water from the volume/pressure controller (12) into the sample. In the objectives of reforming gas hydrates faster, this provides also the same final pressure - temperature conditions for gas hydrates in the end for all tests.
- Step 7 – Depressurization-induced hydrate dissociation: The confining pressure is maintained at 22 MPa while the valve V_2 is opened to decrease the pore pressure. The volume of methane dissociated from the specimen is measured by the system (9) composed also a gas/water separator and a gas collection system.

The steps 3 – 7 are performed in the MRI system and the data are logged automatically during these steps.

2.4. Calibration tests

Calibration tests were performed at 2°C on the compacted specimen of the first test, the density of which was also very similar to that of test 2, saturated with pure phases of various fluids: (a) vacuum; (b) methane gas at 7 MPa of pressure; (c) water at 7 MPa of pressure; (d) and water at 19 MPa of pressure. In Figure 3, *FID INTENSITY* obtained for the whole system in each case is plotted. The values corresponding to methane gas at 7 MPa of pressure, water at 7 MPa of pressure, and water at 19 MPa of pressure were then calculated by subtracting that corresponding to the system containing vacuum, in order to remove the spurious signal owing to the pressure cell and the imperfectly perfluorinated oil. In the working conditions of the present study, and as far as the temperature is not modified, the corrected signal is directly

proportional to the total amount of hydrogen atoms contained in the fluid molecules. The corrected values of *FID INTENSITY* are also plotted in the Figure 3. Note that the signal for pure methane is significantly smaller than that for water due to the different density and chemical composition. In the subsequent sections, the corrected values of *FID INTENSITY*, i.e. *FID INTENSITY* measured minus *FID INTENSITY* obtained from the case (a), are shown.

2.5. Test program

Two tests were performed in this study with the same procedure and the same parameters to ensure the repeatability of the results. The water saturation obtained after compaction equals to 25% (corresponding to a moisture content of 6%).

3. Experimental results and Discussions

3.1. Hydrate creation

Figure 4 (a) shows the evolution of *FID INTENSITY* during hydrate formation (step 3) for the two tests. When methane gas is injected into the specimen, *FID INTENSITY* increases slightly during the first minutes then decreases continuously; the relationship between *FID INTENSITY* and logarithm of time during the decrease phase can be correlated with a linear function. After $t = 40$ h *FID INTENSITY* remains constant. The results obtained by the two tests look similar even if during the first test, the data were not recorded during the first minutes. The increase of *FID INTENSITY* during the first minutes can be explained by the accumulation of methane gas inside the specimen when the gas pressure was increasing until it reached the target value (7 MPa), see Figure 4 (b) where gas pressure is plotted versus elapsed time for Test 2 (data for Test 1 was not available). When the gas pressure exceeds the conditions required to create gas hydrate (3 MPa at 2 °C), gas hydrates start to be created inside the specimen.

This phenomenon decreases the quantity of water and increases the quantity of gas hydrates. That explains why gas hydrate formation decreases the total *FID INTENSITY*. Note that the intensity related to gas hydrate is negligible [31].

The following equation is used to estimate hydrate saturation (S_h):

$$S_h = 1.1 \frac{I_0 + I_m - I}{I_0 + 0.1 \frac{S_{wo}}{1 - S_{wo}} I_m} S_{wo} \times 100\%$$

Where I_0 is the initial FID intensity of the moist sand specimen and S_{wo} is the initial water saturation ($S_{wo} = 25\%$). The remaining void (about 75% of total void) contents methane gas (at 7 MPa of pressure when this pressure is reached). For this reason, I_m - the FID intensity of methane gas (at 7 MPa of pressure) in the specimen before the hydrate formation, equals to 75% of the value obtained from the calibration test (case (b)): $I_m = 0.75 \times 1000 = 750$. This equation is applicable only when the gas pressure equals 7 MPa. The underlying assumption for this equation is that water reacts locally to form hydrates, and that gas can go in and out of the sample to occupy the remaining space between hydrates and remaining water, owing to the 10% of volume increase when water is converted to hydrate. As a result, during the hydrate formation, the remaining void containing methane gas is $(100 - S_{wo} - S_h)\%$ of total void.

Figure 4 (c) shows the estimated hydrate saturation evolution for Test 2. Hydrate starts to be created immediately when the gas pressure is higher than 3 MPa. As mentioned before, hydrate saturation is only calculated from when pore pressure reaches 7MPa (at 0.06th hour, hydrate saturation is 0.3%). The hydrate content increases then linearly with the logarithm of time and reaches its maximal value after 40 h. Note that, after 40 h, $S_h = 27\%$, that means all water in the specimen has been transformed to hydrate,

and that the remaining NMR signal at the end of the process is that of the methane phase.

Figure 5 plots the signal (*i.e.* owing to water and methane) versus the elevation ($Z = 0$ corresponds approximatively to the bottom of the specimen) for various times. It can be noted that the signal is generally homogenous along the specimen elevation. At the beginning ($t = 0$), the specimen contains only water and air in the pore space. Slight fluctuation of the signal along the elevation should correspond to the compaction procedure (moisture sand tamped by layers of 10 - 20 mm), which induces slight heterogeneity of porosity and water distribution in the specimen. When methane gas is injected into the specimen, GH is formed and the water content decreases progressively. That explains why the signal decreases progressively with time and the profile becomes more homogenous.

Bagherzadeh et al. [33] found that hydrate formation occurs faster in a bed with lower initial water saturation and as opposed to the higher water saturation case, hydrate formed homogeneously at 25% of initial water saturation. This is in agreement with homogenous Z profiles during GH formation in gas saturated media in this study.

Rydzy [34] investigated the kinetics of methane hydrate formation in unsaturated Ottawa sand via the combination of wave velocity measurements and MRI (Mean Intensity, MI). The results showed that at low initial water saturation, MI decreased quickly few hours after gas injection which means hydrate saturation increased quickly. In addition, velocities (compressional and shear velocities) increased quickly during hydrate saturation, slowed down and became stable from when hydrate formation was

almost finished. This could be explained by cementation model illustrating hydrate growth in capillary water at sand grains contacts [37,38] which supposed that films of hydrates are first formed quickly at water-gas interfaces, the subsequent hydrate formation (from the films toward the centers of grain contacts) is slower depending on the diffusion of methane molecules through the hydrate film and water. This can be also used to explain the linear relationship between *FID INTENSITY* and logarithm of time observed in the present study during the hydrate formation. However, in the work of Rydzy [34], 5% to 12% of pore water was found to remain unconverted to hydrate at the end of experiments while in the present study almost 100% of water becomes hydrates. Actually, in the work of Rydzy [34], the signal of methane gas was not considered and that would induce errors in water content estimation in the specimen.

3.2. Water Saturation

Figure 6 plots *FID INTENSITY* during the water saturation (Step 4). $t = 0$ corresponds to the opening of the valve V_2 . That induces a quick decrease of *FID INTENSITY* to 0. Afterward, when water is injected to the specimen ($t = 0.06$ h) *FID INTENSITY* increases quickly and reaches the maximal value when water pressure reaches 7 MPa. Water injection in Test 1 is slowed down between 0.1 – 0.4th hour due to an interruption to inject more water into the volume/pressure controller (12).

The signal versus elevation is plotted at various times for the Test 2 in Figure 7. Profile at 60s ($t = 0.047$ h) was measured when methane gas was decreased to the atmospheric pressure. When water is injected from the bottom inlet, signal at the bottom starts to increase first ($t = 0.063$ h). When the water pore pressure reaches 7 MPa, the specimen can be expected to be fully saturated with water, $t = 55$ h (methane

gas should not exist in this conditions). At this state, higher signal can be observed in the zone close to the bottom of the specimen while it is lower in the zone close to the top.

Figure 8 plots the signal versus elevation for both two tests at the end of the water saturation step. The results of the Test 1 show also a higher signal close to the bottom but the signal at the top is similar to the remaining part of the specimen. The heterogeneity of water distribution at the end of this step can be explained by the saturation procedure. Actually, methane gas evacuation and water injection were performed both from the bottom. Methane gas evacuation, even if it was performed quickly, less than one minute, would induce hydrate dissociation at the zone close to the bottom. That explains why in the end, hydrate saturation at the bottom was lower (higher signal) than the other parts of the specimen.

Hydrate saturation is estimated 20.5% and 27.5% respectively for two tests based on intensity of water saturated sample at 7MPa. Hydrates dissociation at the zone close to the bottom induces eventually the decrease of hydrate saturation compared to that after hydrate creation step. However, it is the same for Test 2. When water is injected from the bottom, the remaining gas would cumulate in the zone close to the top of the specimen, thus impeding total water saturation. At the end of water saturation phase, remaining gas would be transformed to gas hydrates, hydrate saturation in increased. That is why the hydrate saturation in this zone seems higher than in the other parts (lower signal) in Figure 8.

3.3. GH Dissociation-Reformation

As mentioned above, a temperature cycle was performed after the water saturation phase. Figure 9 shows the pore pressure (a), the cryostat temperature (b) and *FID INTENSITY* (c) versus elapsed time for Test 1. It should be noted that specimen temperature could not be measured during these tests in the MRI system. However, preliminary tests performed outside the MRI system showed a characteristic time of 20 min for the temperature exchange between the cryostat and the specimen. At the beginning of the tests, the pore pressure is first decreased to 4 MPa for a faster heating-induced gas hydrate dissociation as gas hydrates are closer to equilibrium boundary. Note that heating gas hydrates in undrained conditions induced the increase of pore pressure (close to corresponding equilibrium pressure of gas hydrates) mainly due to thermal dilation of water and hydrate dissociation [39]. Afterward, the cryostat temperature is increased from 2 °C to 25 °C with a constant rate. As heating is performed under undrained conditions (the valves V_1 and V_2 were closed), pore pressure increases according to heating and stabilizes at 14 MPa when the temperature reaches 25 °C. Heating-induced pore pressure increase is mainly due to thermal dilation of water and hydrate dissociation [39]. After this phase, the valve V_1 is opened to connect the cell to the pressure/volume controller (No. 12 in Figure 2) in order to impose a pore pressure of 19 MPa. This pressure is maintained until the end of the cooling-induced hydrate re-formation phase (Step 6). At $t = 7.5$ h, the cell temperature is decreased quickly to 2 °C to re-create GH.

Figure 9 (c) plots *FID INTENSITY* versus elapsed time during these steps. The data from the beginning to $t = 1.6$ h was unfortunately not available. From $t = 1.6$ h, *FID INTENSITY* decreases as the specimen temperature increases. Note that owing to

Curie law for spin polarization in the MRI magnet, *FID INTENSITY* must be here considered to be additionally influenced by temperature, being inversely proportional to its absolute value in Kelvin. For a given fluid content, it then increases when temperature decreases and vice versa. At $t = 2.8$ h, *FID INTENSITY* starts to increase when the signal of water creation (from dissociated GH) was higher than that induced by temperature increase. In the present study, no direct temperature measurement was available inside the specimen, and no temperature correction of *FID INTENSITY* was made. At $t = 3.6$ h, *FID INTENSITY* decreases when GH has been completely dissociated (pore pressure reached 14 MPa) but the specimen temperature continues to increase to reach the imposed temperature in cryostat. At $t = 4.4$ h, increasing pore pressure from 14 MPa to 19 MPa induces an increase of *FID INTENSITY*. When the cryostat temperature is decreased quickly ($t = 7.5$ h), the temperature of the specimen decreases progressively inducing an increase of *FID INTENSITY*. At $t = 8.2$ h, GH starts to be re-created progressively inducing decrease of *FID INTENSITY*. When the GH re-creation is completed, *FID INTENSITY* stabilizes.

The results of the Test 2 are shown in Figure 10. After reducing the pore pressure from 7 MPa to 4 MPa, the cryostat temperature is increased quickly from 2 °C to 20 °C ($t = 0.1$ h) and then to 25 °C ($t = 2.1$ h). It is decreased to 2 °C at $t = 22$ h. Heating under undrained conditions induces an increase of pore pressure from 4 MPa to 15 MPa. The subsequent heating (from 20 °C to 25 °C) does not influence the pore pressure. From $t = 4.1$ h, the pore pressure is maintained at 19 MPa as the case of the Test 1. The results on *FID INTENSITY* show phenomena similar to that observed in Test 1: $t = 0 - 0.6$ h, *FID INTENSITY* decreases due to heating; $t = 0.6 - 1.9$ h, *FID INTENSITY* increases due to GH dissociation; $t = 1.9 - 4$ h, *FID INTENSITY* decreases due to

heating; from $t = 4$ h, *FID INTENSITY* increases due to increase of pore pressure (from 14 MPa to 19 MPa); $t = 22$ h *FID INTENSITY* increases first due to cooling then decreases due to GH re-formation. More regular *FID INTENSITY* acquisitions between 2-5th hour are not available to reflect better the GH dissociation – reformation.

Figure 11 shows the signal versus elevation for the two tests at the end of the water saturation, GH dissociation, and GH reformation phases. The results show a slight redistribution of water after the GH dissociation/reformation cycle. At the end of this cycle, water seems distributed more homogeneously. Min/Mean and Max/Mean profile signal of Test 1 are (0.92; 1.30), (0.93; 1.10) respectively for water saturation and GH reformation case. Similarly, they are (0.76; 1.32), (0.90; 1.26) for Test 2.

3.4. Depressurization-induced hydrate dissociation

To observe the depressurization-induced GH dissociation, pore pressure is first decreased from 19 MPa to 5 MPa while specimen temperature is maintained at 2 °C. Note that, these conditions are inside the GH stabilization zone. The valve V_2 is then connected to the system (9) while the valve V_1 is closed. That reduces pore pressure directly to atmospheric pressure. The quantity of dissociated methane gas measured by the system (9) is used to estimate the hydrate saturation S_h remaining in the specimen. MRI data are disregarded for such purpose because ice is likely to appear in the specimen at this step and impede the direct interpretation of signal intensity.

Figure 12 shows hydrate saturation and *FID INTENSITY* versus elapsed time during the GH dissociation for Test 1 (a) and Test 2 (b). The results of Test 1 show a quick decrease of S_h from 21% at the beginning to 0 almost after 0.2 h. During this period,

FID INTENSITY decreases quickly. Once the hydrate dissociation is finished, *FID INTENSITY* increases slowly during the next hour. The results of Test 2 show similar trends but *FID INTENSITY* decreased more slowly at the beginning. In fact, in the objective of decelerating the gas hydrate dissociation, for Test 2, valve V_2 was opened partly at the beginning (0 - 0.067^h hour). However, hydrate dissociation was stopped as created gas and water were blocked in the sample. Valve V_2 was so opened completely, *FID INTENSITY* decreased fast afterward. The decrease of *FID INTENSITY* during the hydrate dissociation phase can be explained by the expellee of water from the specimen by the created methane gas. At the same time, as hydrate dissociation is an endothermic process, ice would be formed during this phase. That induces decrease of *FID INTENSITY* even when gas hydrates are almost dissociated. In the subsequent phase, ice melting increases the quantity of liquid water in the specimen, which explains the increase of *FID INTENSITY*.

The signal versus elevation is plotted for various times during this step in Figure 13. These results confirm the statement above. Ice formation takes place only in the zone where hydrate is present (that means along the specimen except the zone close to the bottom). For this reason, signal at this zone increases at the end of the dissociation phase (which corresponds to ice melting) while the signal at the zone close to the bottom remains constant. Actually, rapid dissociation by depressurizing the sediments below the quadruple point of methane hydrate drops the temperature below the freezing point of water causing ice formation [9,10]. Heat of hydrate dissociation is 450 Jg⁻¹ [40] while it is -342Jg⁻¹ for the transformation of water at 2 °C to ice. Depending on heat transfer in the temperature control system to compensate the temperature decrease due to GH dissociation, GH reformation and ice formation ratio vary

depending also on the kinetics of GH dissociation. That is why, pore pressure is reduced from 19 MPa to 5 MPa before finally set up at atmospheric pressure to better observe the GH dissociation. Fan et al. 2017 [35] investigated the methane hydrate dissociation in glass beads by depressurization method. Ice formation was also observed by a rapid reduction of M/I and water distribution variation with time in the case where pore pressure was reduced below the quadruple point of methane hydrates.

To exploit natural gas hydrates after the depressurization method, the pressure in a bottom hole is first lowered by a submersible pump. During the GH dissociation, GH saturation decreases, low pressure is transferred to a distant region from well due to dramatic increase of permeability. GH dissociation stops when reservoir temperature is lower or identical to the corresponding GH equilibrium due to an endothermic reaction [14]. GH reformation and/or ice formation during GH dissociation is a common problem to overcome to increase the potential of hydrate production after the depressurization method. Some reservoir simulators (Hydrosim, MH 21, STOMP-HYD, CMG-STARs, TOUGH + HYDRATE) have been developed and are commonly used [14]. However, field scale production tests are needed to improve the accuracy of numerical predictions. In this study, due to the limited laboratory specimen size, the high production pressure and the fast depressurizing rate, the dissociation and ice formation are observed almost homogenous along the elevation. Experimental scale is then one of the important factors needed to be paid attention for future laboratory GH dissociation studies.

Conclusion

MHBS is firstly created by pressurizing methane gas (at 7 MPa) into already chilled moistened packed sand specimen (after excess gas method). Following the hydrate formation, water is injected into the specimen and the remaining gas is bled out simultaneously. A subsequent heating/cooling cycle is applied in order to completely dissociate GH and then recreate them inside the specimen. Methane hydrate dissociation after the depressurization method is also investigated after the whole GH formation process. From MRI measurements, the following conclusions can be drawn:

- Pressurizing methane gas into already chilled moistened packed sand specimen creates GH homogenously in the specimen. The formation is fast at the beginning, slows down after some hours and then stabilizes after some ten hours.
- Subsequent water saturation redistributes GH in the specimen. S_h at the water inlet is smaller than the other part (due to GH dissociation) while S_h at the opposite end could be higher (due to additional GH formation).
- Undrained heating/cooling cycle makes the GH distribution more homogenous in the specimen.
- The ice formation due to depressurization-induced GH dissociation below the quadruple point of methane hydrate is observed.

The findings of the present work would be helpful for future studies on MHBS in laboratory. The temperature cycle is considered as an essential step to reproduce natural MHBS homogenously in the specimen. MRI is a good mean to investigate the hydrate dissociation.

Acknowledgement

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Table 1. Characteristics of Fontainebleau sand [41]

Material	d ₅₀ (mm)	d ₁₀ (mm)	e _{min}	e _{max}	Angularity	ρ _s (Mg/m ³)
Fontainebleau sand	0.206	0.150	0.56	0.88	Sub-rounded	2.65

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d₁₀, d₅₀: grain sizes corresponding to 10, 50 % passing respectively; e_{min}, e_{max}: minimum and maximum void ratio respectively; ρ_s grain mass density.

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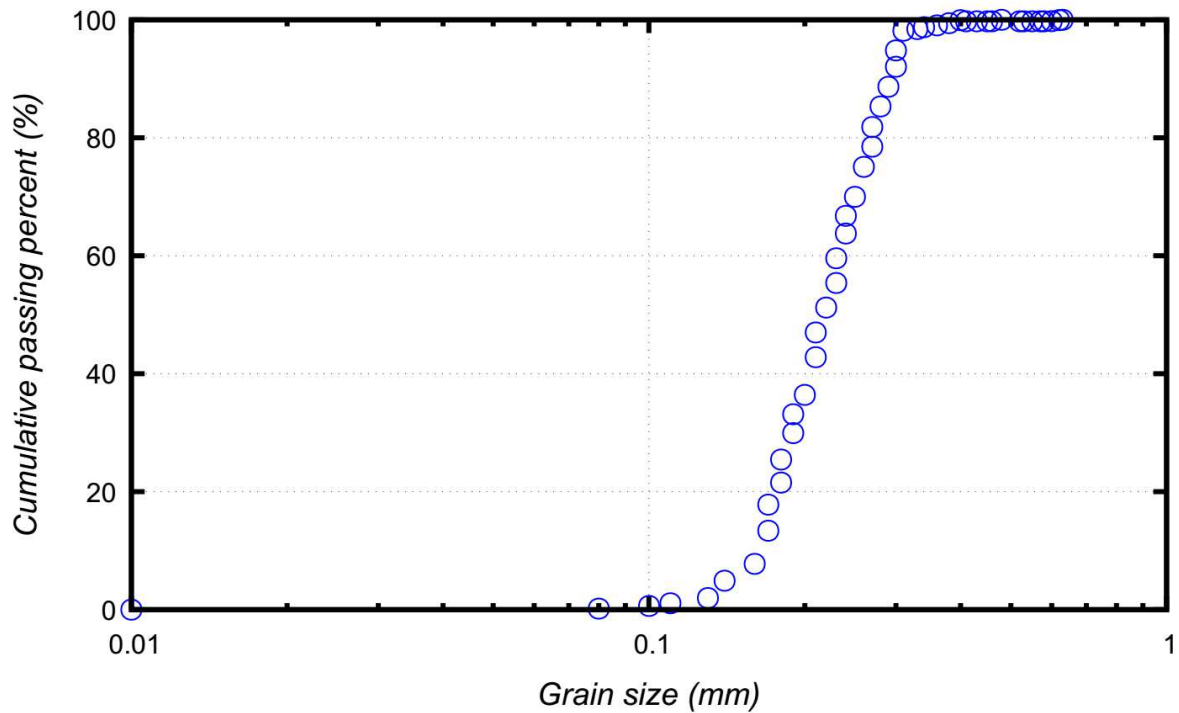
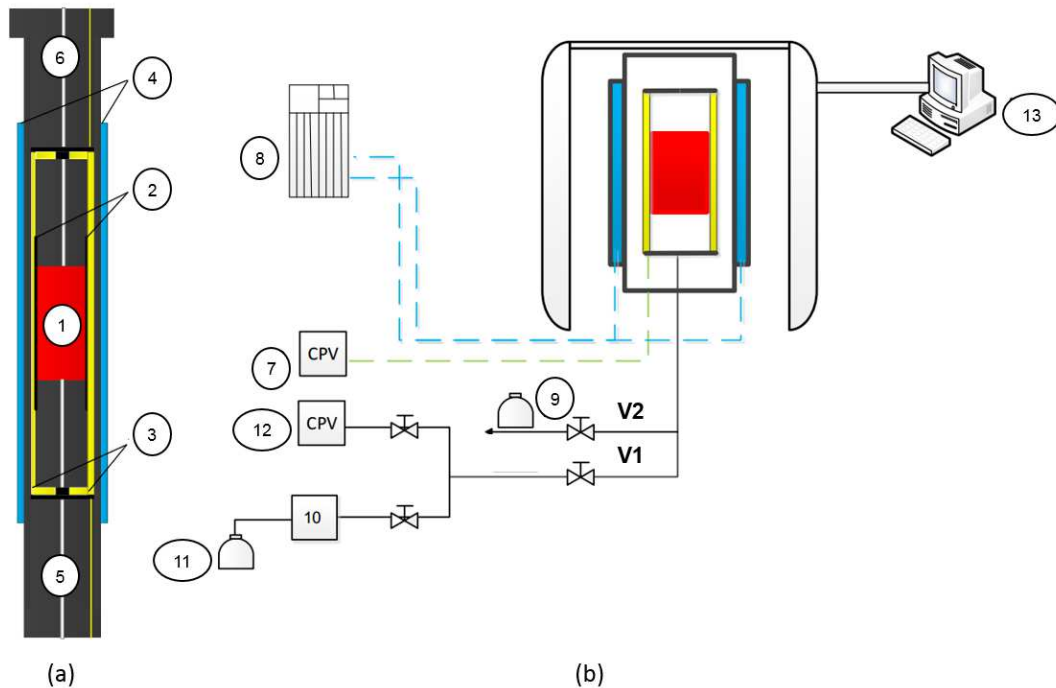


Figure 1. Particle size distribution (modified from [37])



1 - Sand specimen; 2 - Neoprene membrane; 3 - Confining fluid; 4 - Temperature controlling fluid; 5 - Bottom inlet; 6 - Top inlet; 7 - Confining CPV; 8 - Cryostat; 9 - System to measure volume of gas; 10 - Gas flowmeter; 11 - CH₄ bottle; 12 - Water CPV; 13 - MRI measured system.

Figure 2. Schematic diagram of the experimental setup

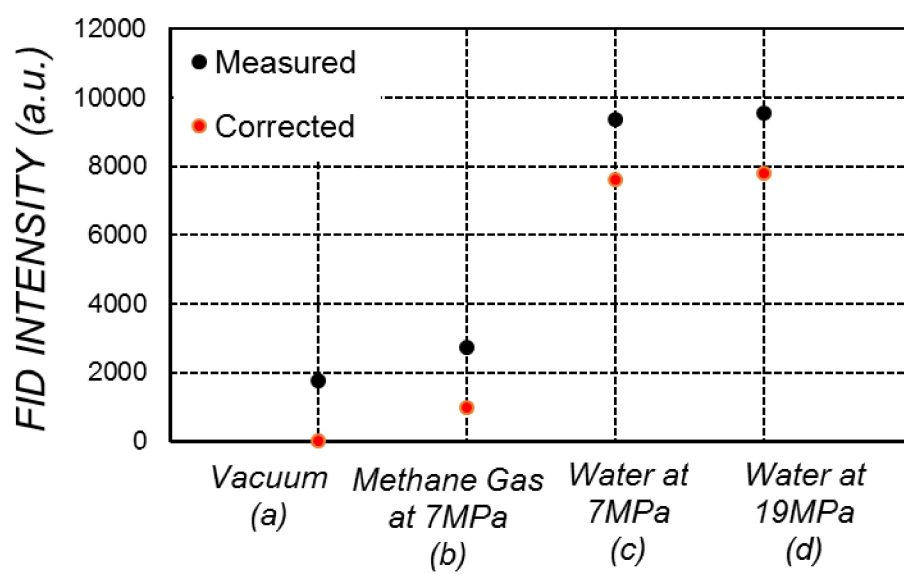


Figure 3. Reference signal

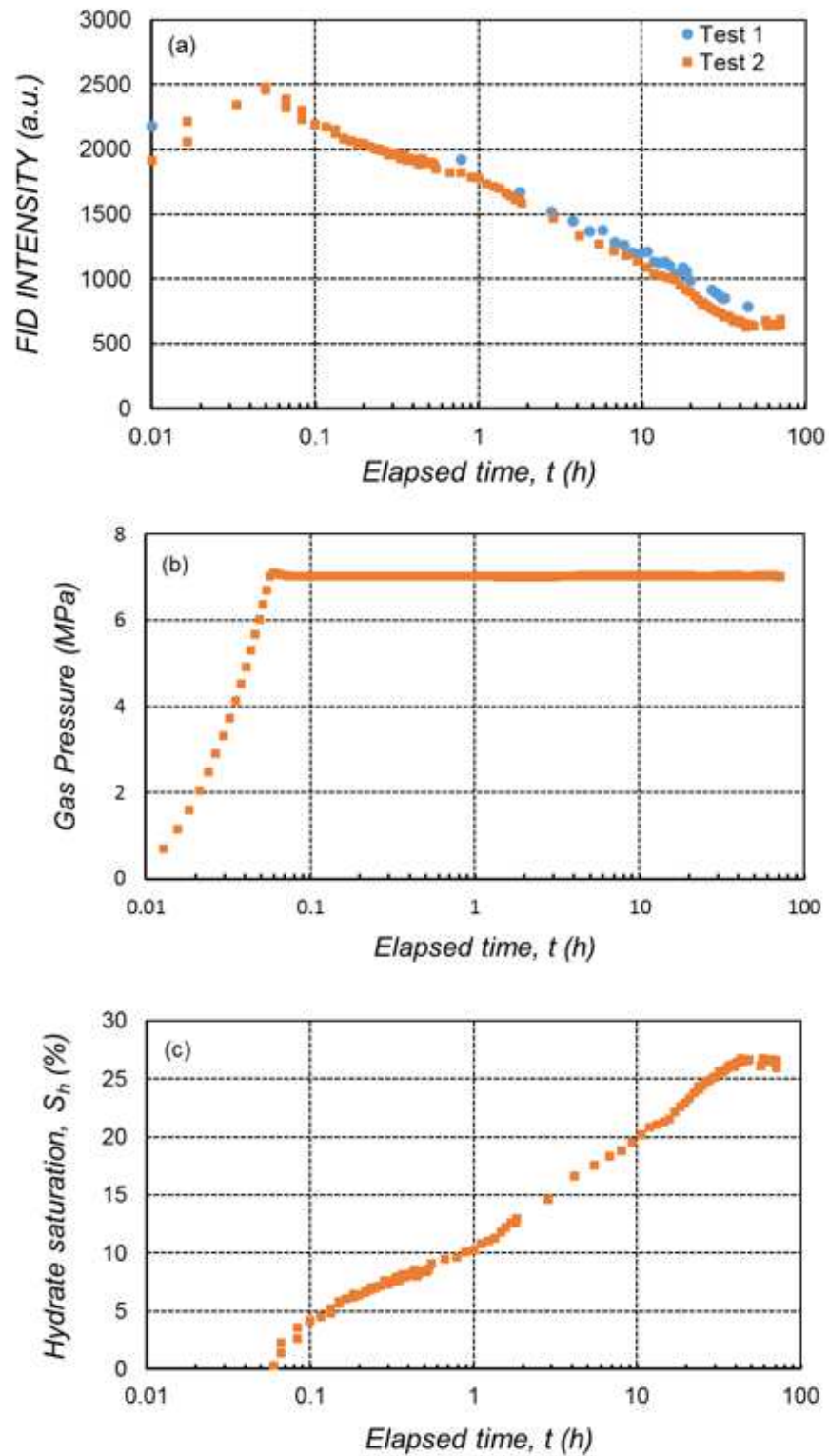


Figure 4. (a) FID Intensity evolution of the two tests during GH Formation in gas saturated media; (b) Pore Pressure and (c) Estimated gas hydrate saturation evolution of Test 2.

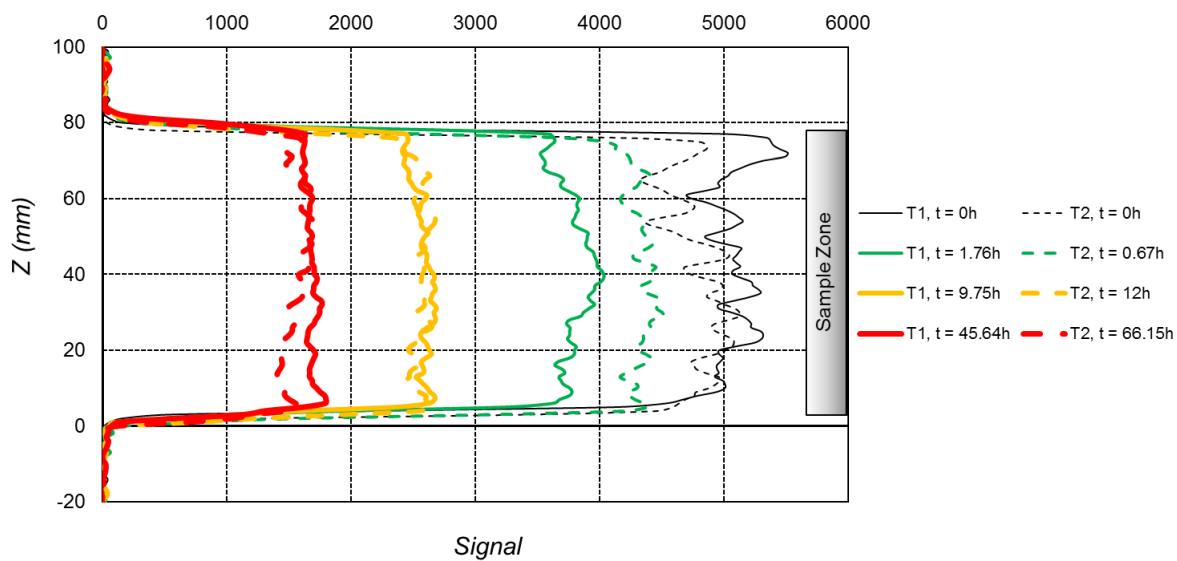


Figure 5. Signal versus elevation for the two tests during GH formation in gas saturated media

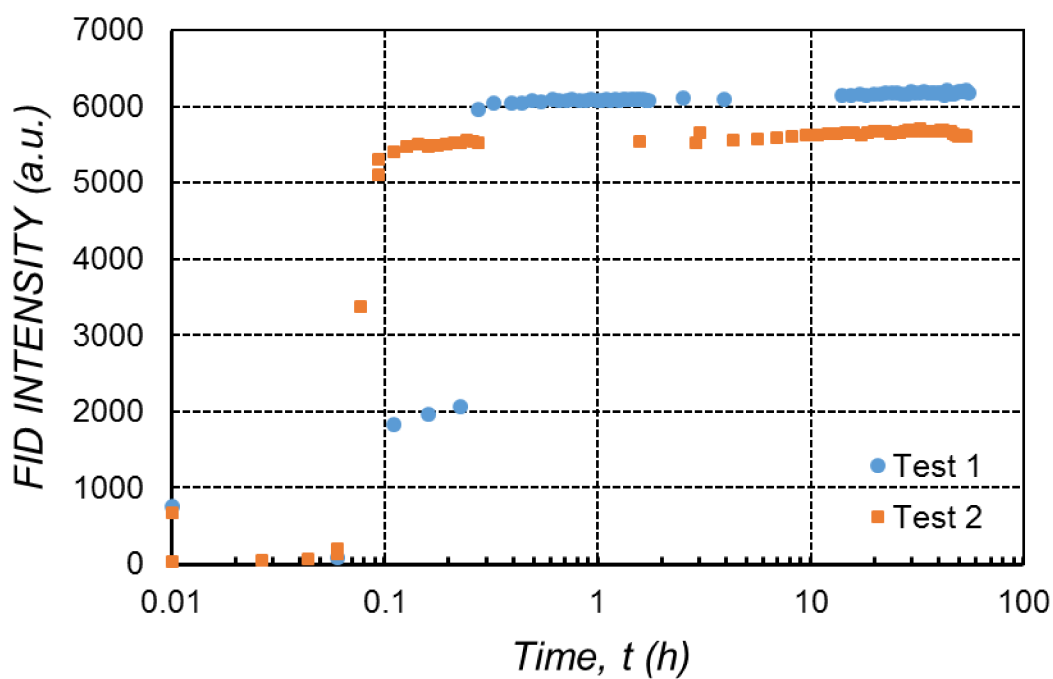


Figure 6. FID Intensity evolution of the two tests during the water saturation process

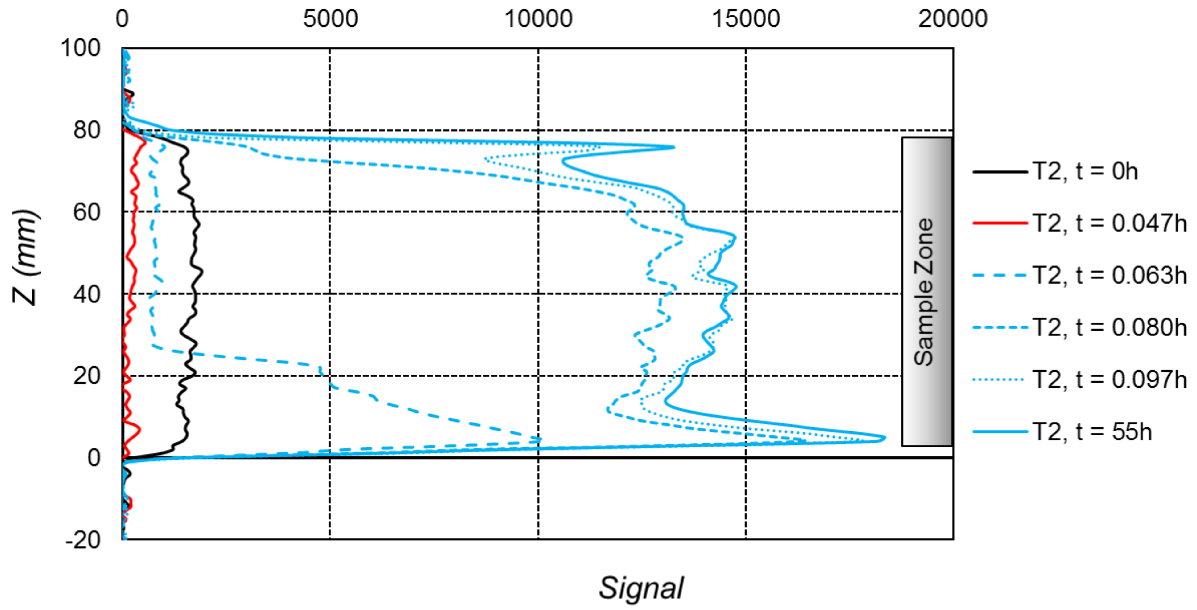


Figure 7. Signal versus elevation for Test 2 during the water saturation process

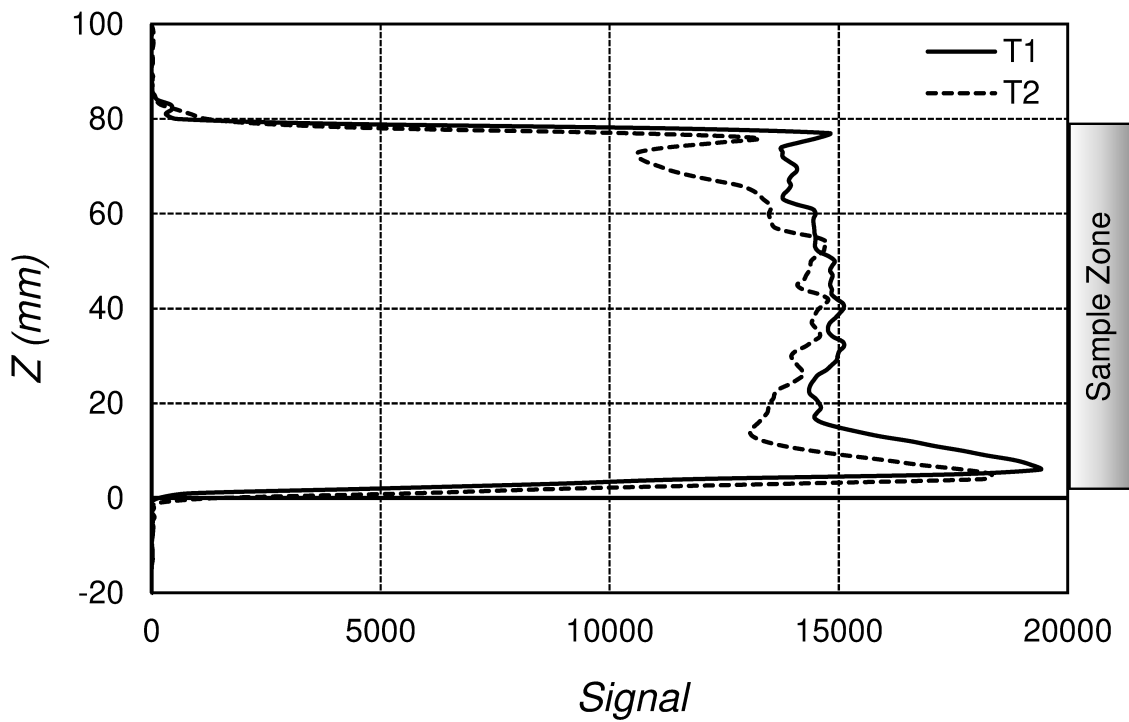


Figure 8. Signal versus elevation for the two tests at the end of the water saturation phase

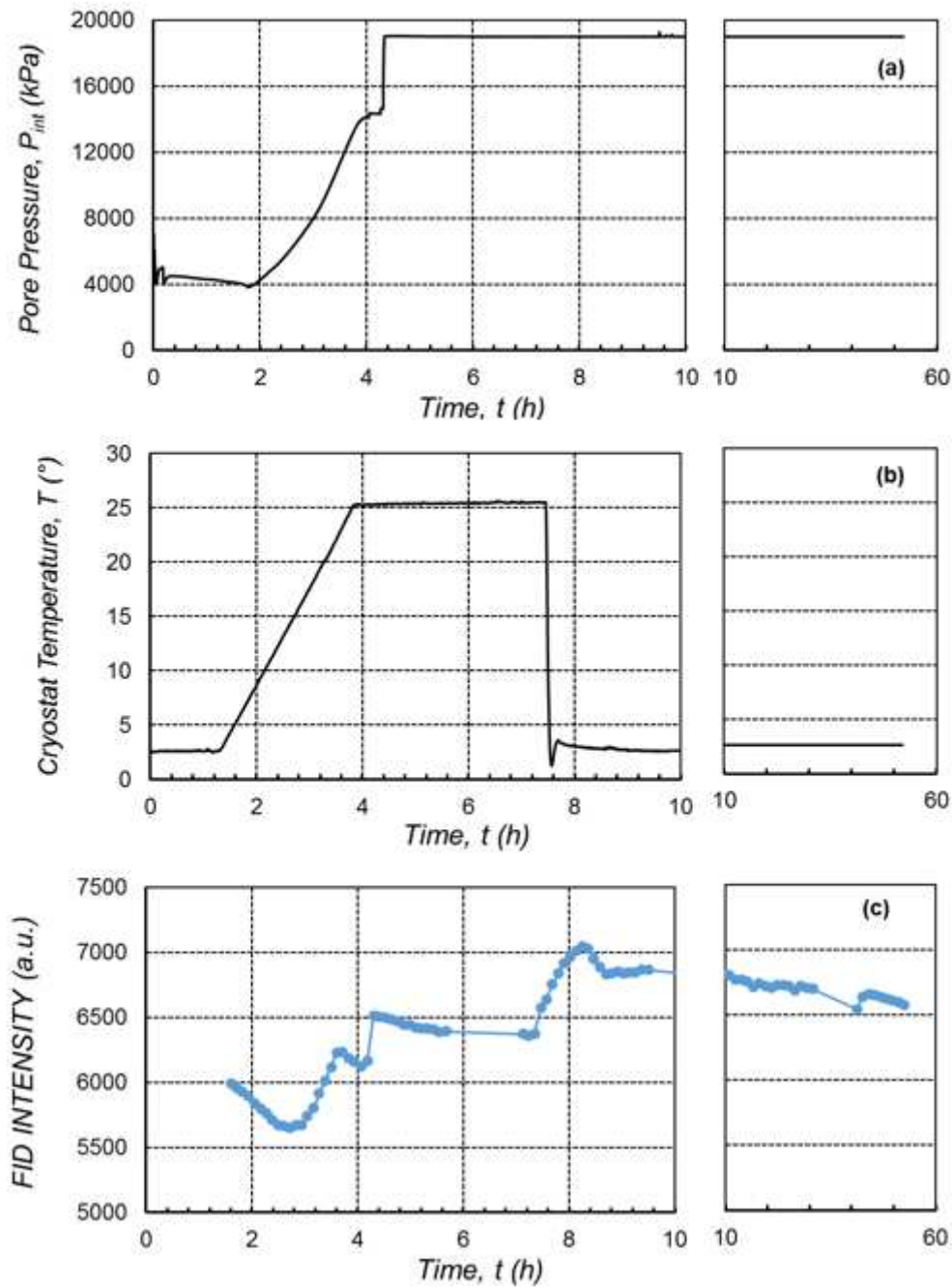


Figure 9. (a) Pressure evolution; (b) –Temperature evolution; (c) FID Intensity evolution during GH dissociation-reformation of Test 1

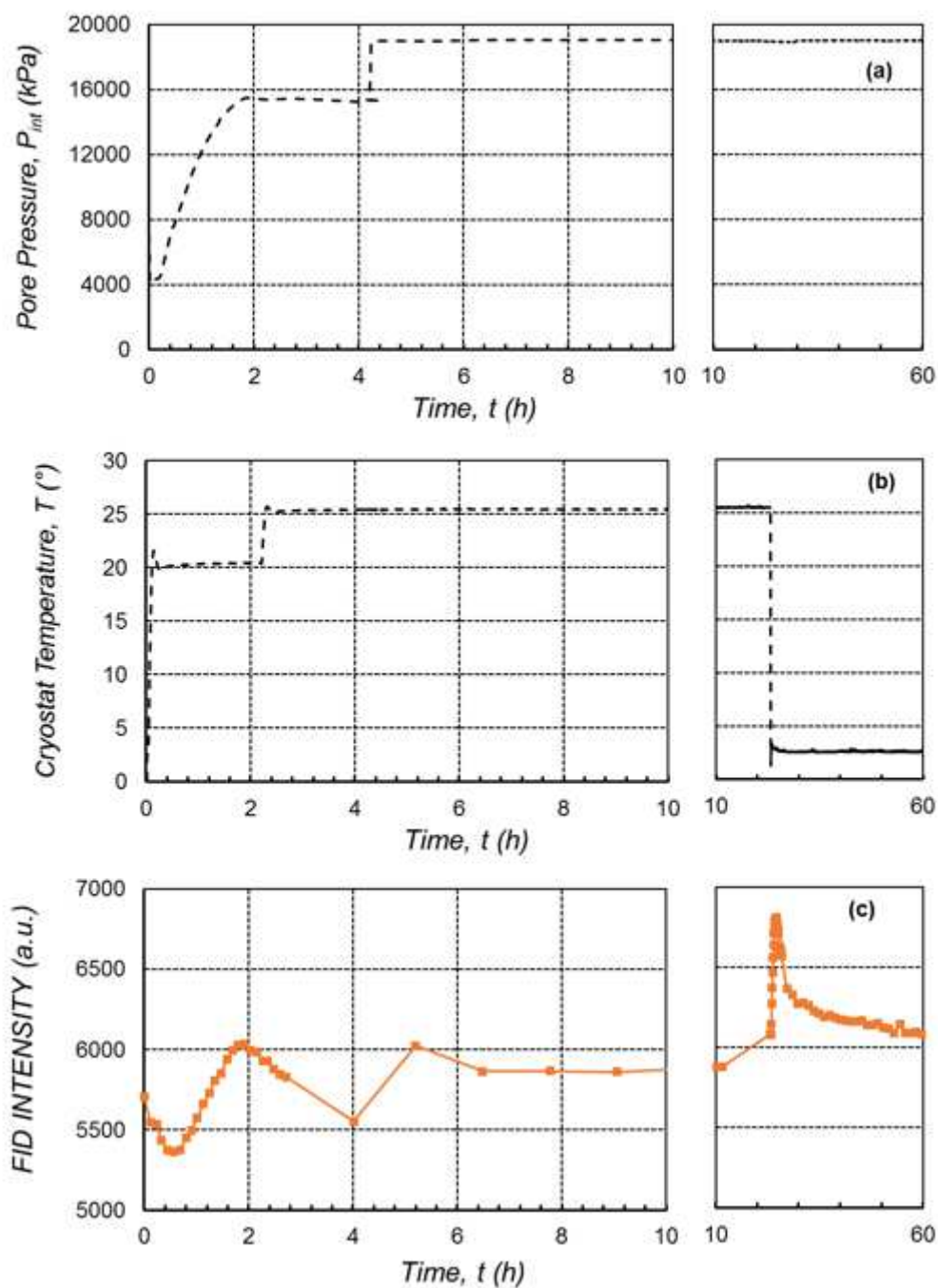


Figure 10. (a) Pressure evolution; (b) Temperature evolution; (c) FID Intensity evolution during GH dissociation-reformation of Test 2

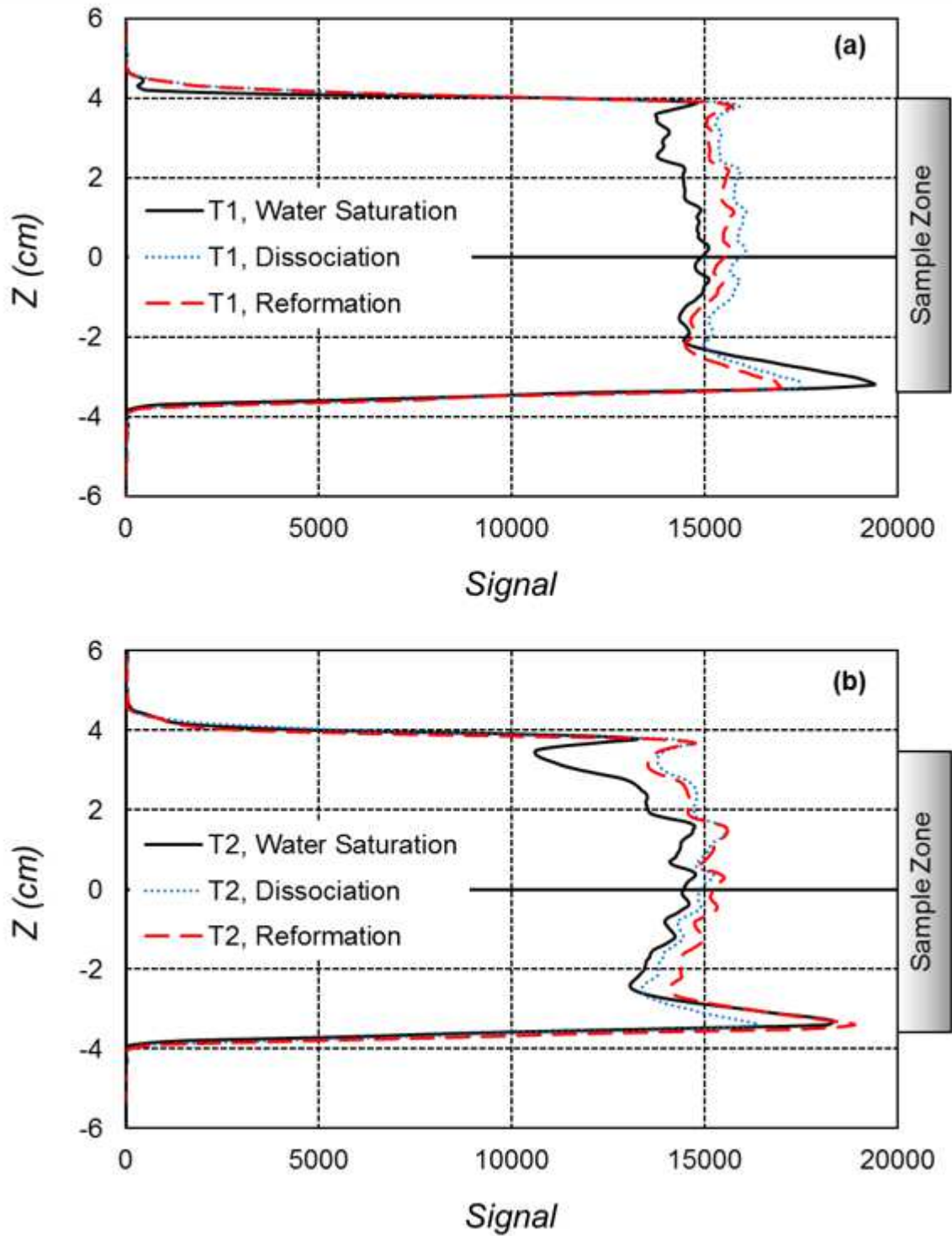


Figure 11. Signal versus elevation at the end of the water saturation, GH dissociation, and GH reformation phases: (a) Test 1; (b) Test 2.

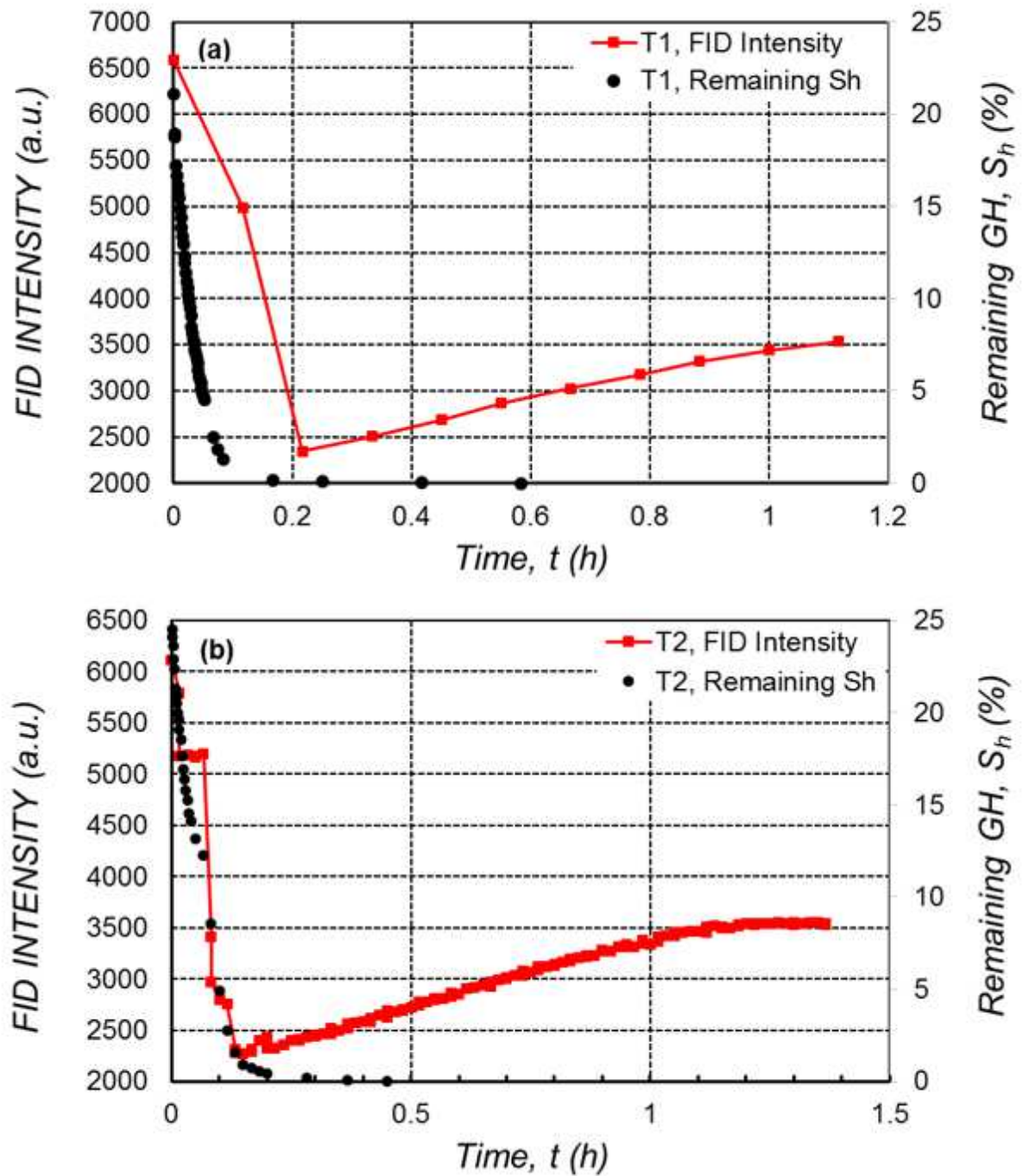


Figure 12. FID Intensity and Remaining GH evolution during GH dissociation for (a) Test 1 and (b) Test 2.

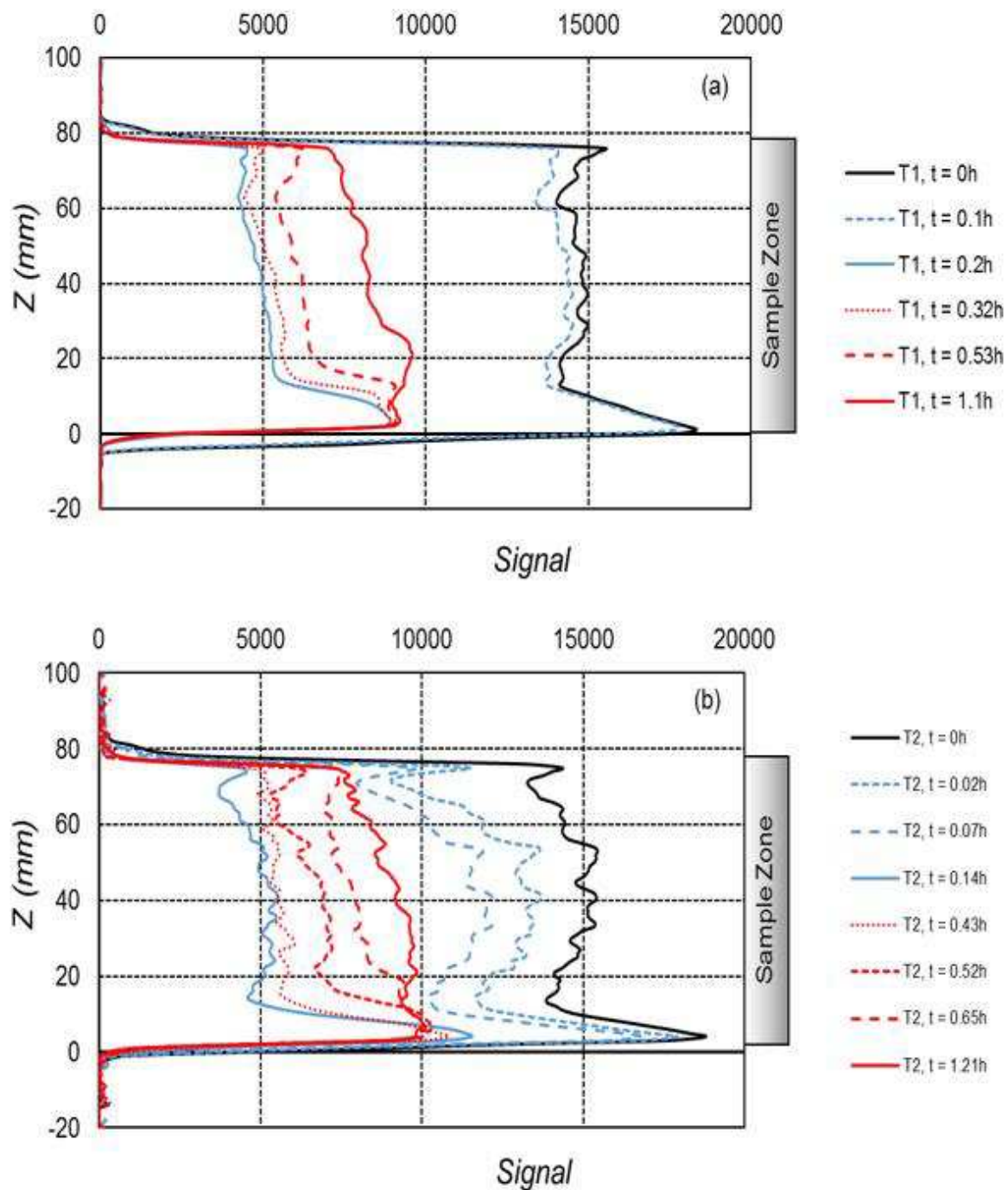


Figure 13. Signal versus elevation for the two tests during GH dissociation